

# TIFONE: a design-oriented code for the inter-wrapper flow and heat transfer in liquid metal-cooled reactors



**Politecnico  
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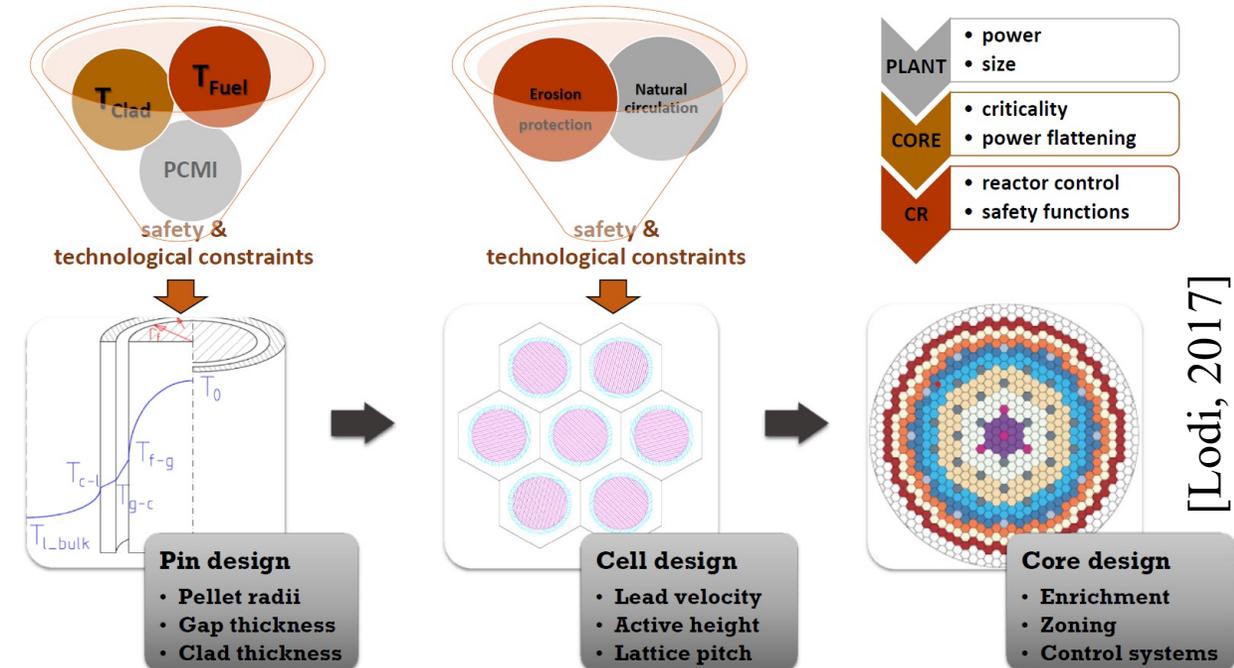
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Thermal Hydraulics of Fast Reactors*  
@ C. R. ENEA, Camugnano, Italy

# LFR core design - the need for dedicated tools

- A comprehensive approach to core design:
  - Identify **safety and technological constraints** → derive **design guidelines**
  - Design individual components
  - Manage interfaces with other reactor systems
  - **Optimize performance by working on available margins**
- Computational tools in support of core design:
  - **Design-Oriented Codes (DOCs):**
    - Target: **equilibrium**
    - Balanced error contributions, fast-running
    - Clear application domain
  - Verification-Oriented Codes (VOCs):
    - Target: **high accuracy**
    - Comprehensive physical treatment
    - Sophisticated models and methods

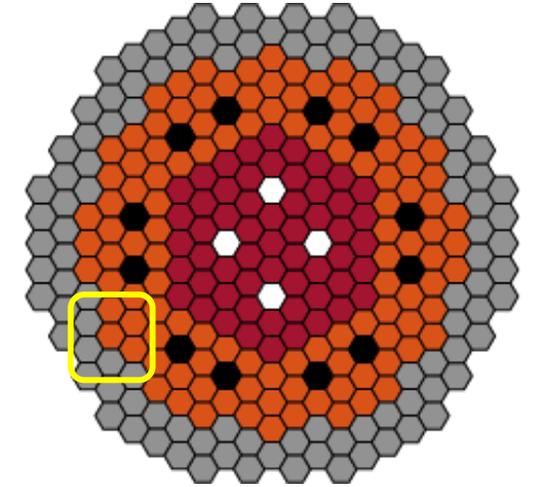
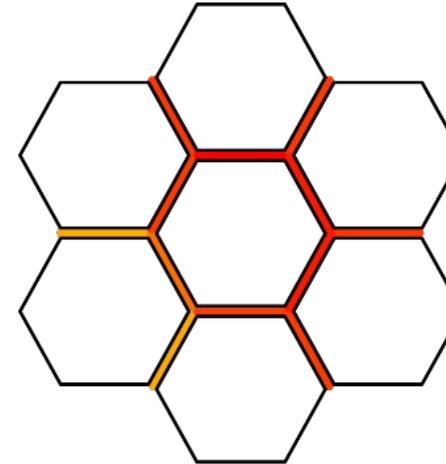


[Lodi, 2017]

- Three “pillars” for core design:
  - Neutronics (NE)
  - Thermal-hydraulics (TH)
  - Thermo-mechanics (TM)

# Motivation to develop a new code: TIFONE, a DOC for LFR core TH

- **Inter-Wrapper (IW) region** is inherent in LFR design (width established by core TM design)
    - Among the core TH design goals: to avoid cold by-passes and excessive thermal gradients among opposite faces of the assembly ducts (**bowing**)
    - To be achieved by working on: IW coolant flow
  - → Core TH design requires knowledge of:
    - **Full-core** axial and radial coolant temperature distribution
    - Axial and perimetrical wrapper temperature profile for each SA
  - Literature review:
    - COBRA-WC, NETFLOW
    - SUPERENERGY-2, SE2-ANL
    - **No available DOC for core TH design (\*)**
- (\* Note on ANTEO+ and porous medium approach



**TIFONE: Termo-Idraulica delle Fughe che Occorrono nel Nocciolo fra gli Elementi**  
*(thermal-hydraulics of the bypass flow occurring in the core among the SAs)*

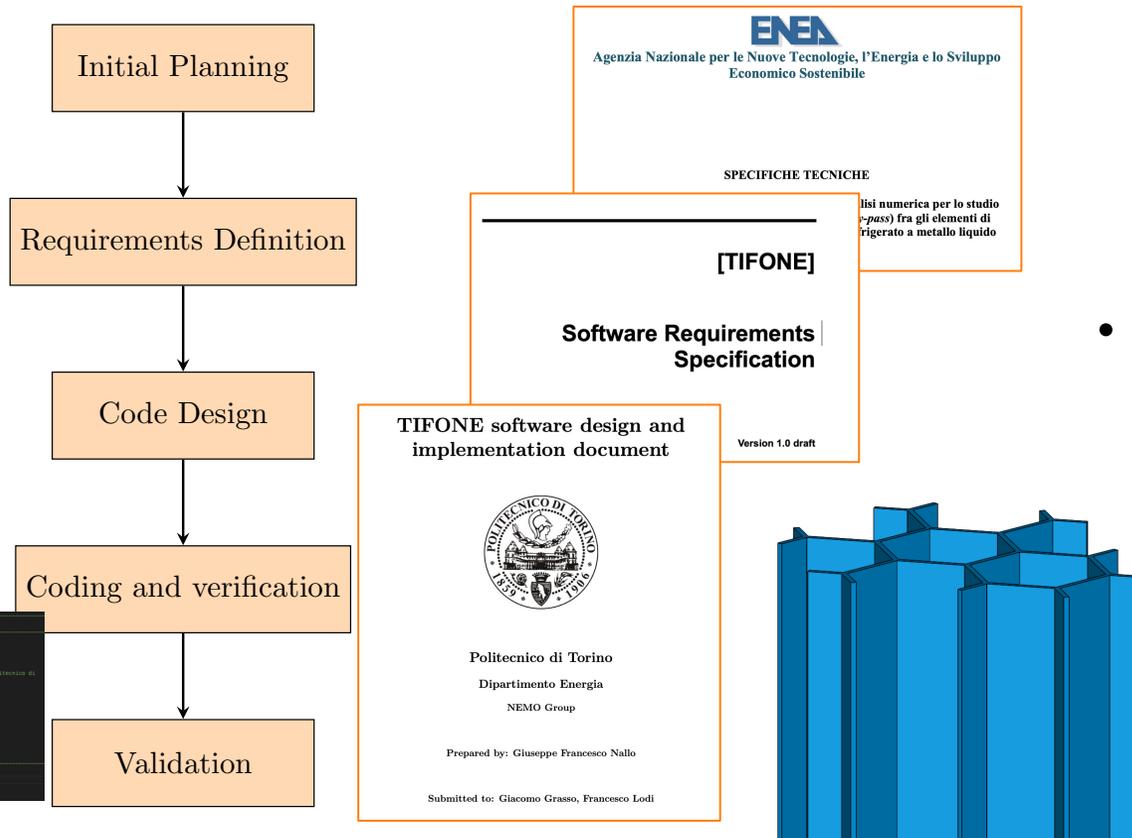
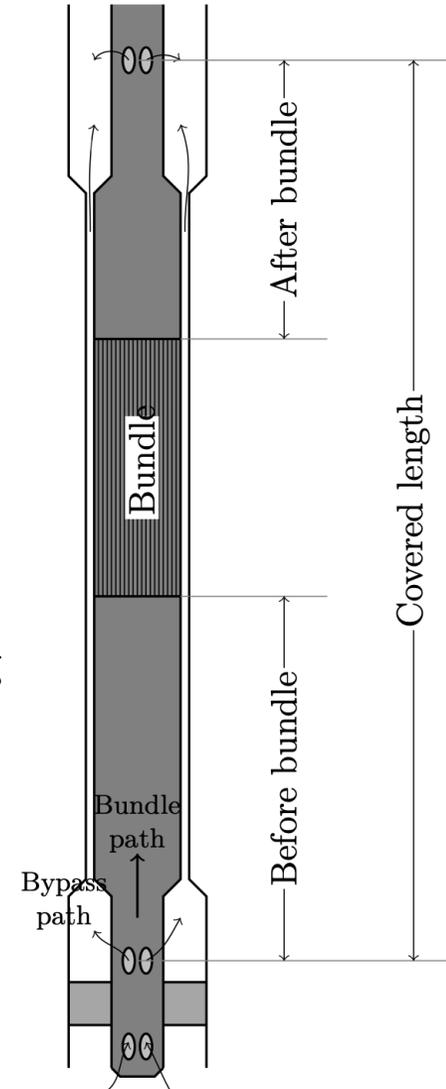
# A quality-compliant code design approach for TIFONE

- TIFONE was developed according to ENEA's **Software Quality Management System** → necessary if intend to use the code to support licensing

- Application domain:
  - Steady-state
  - Liquid metal coolant (\*)
  - Closed, hexagonal SAs
  - Forced and mixed convection regimes (not purely natural circulation)

- Calculation domain:
  - Axially: between dividing and merging of inter- and intra-SA flows
  - Radially: IW region of the entire core

(\*) Na, Pb or PBE

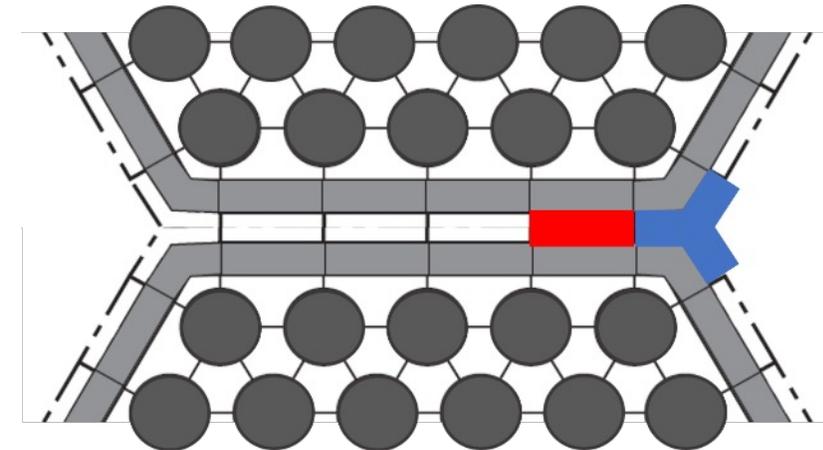
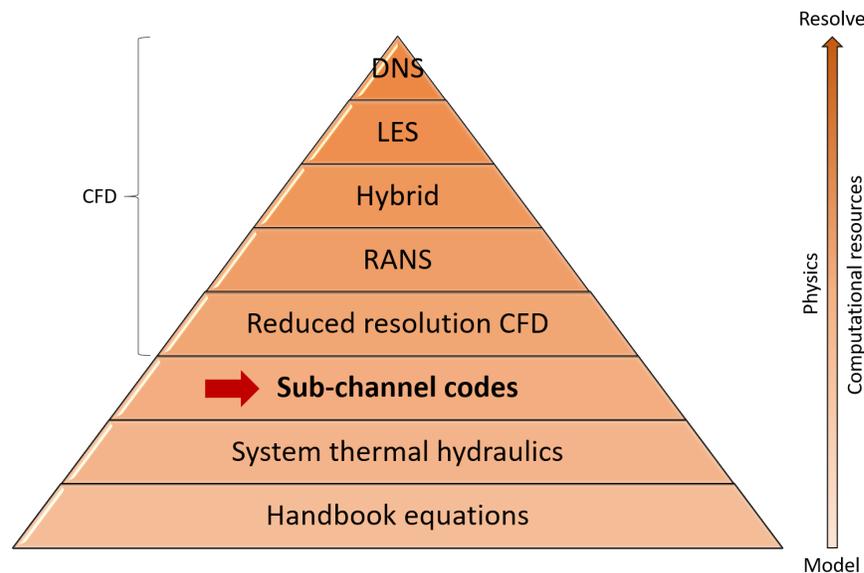


# Problem solving approach and spatial discretization



- Based on the requirements specification, need to select the most suitable calculation approach
- The **Sub-Channel (SC)** method was selected → balance between complexity and accuracy

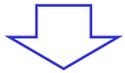
- Spatial discretization:
  - Axial: arbitrary node distribution
  - Radial: arbitrary number of *edge SCs* + one *corner SCs* for each corner.



# Physico-mathematical model: mass conservation



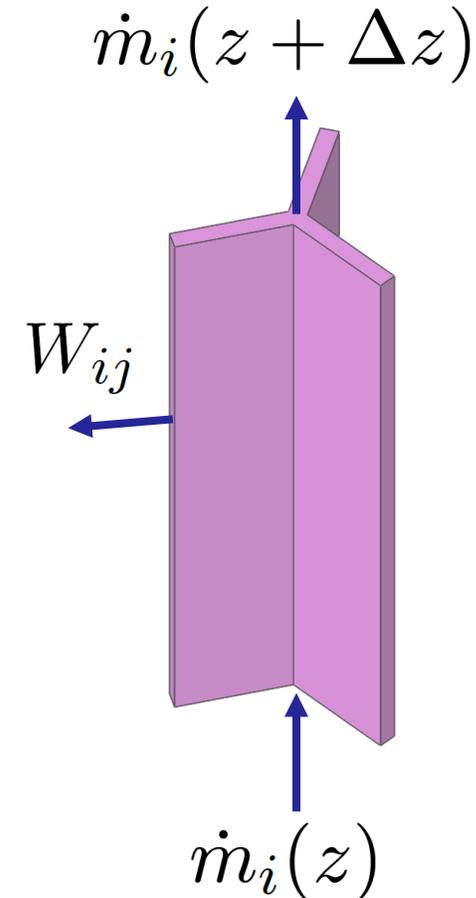
$$A_i \Delta z \frac{\partial}{\partial t} \langle \rho_i \rangle + \Delta \dot{m}_i = -\Delta z \sum_{j=1}^{N_{nei,i}} W_{ij}$$



$$\frac{\Delta \dot{m}_i}{\Delta z} = - \sum_{j=1}^{N_{nei,i}} W_{ij}$$

- Forced convection: neglect inter-SC mass transfer
- Mixed convection: assume inter-SC mass transfer entirely due to buoyancy effects
- Onset of mixed convection for  $Y_{mix} = Gr/Re^2 > 0.002$  [Jackson]

- Boundary condition:  $\dot{m}_{in}$ . User provides  $\dot{m}_{in,core}$  and  $f_{BP}$ ; repartition among SCs is then computed via *flow split* calculation

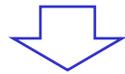




# Physico-mathematical model: energy conservation



$$A_i \Delta z \frac{\partial}{\partial t} [\langle \rho h \rangle_i] + \Delta [\dot{m}_i \{h_i\}] = A_i \Delta z \dot{q}_{eq,i} - \Delta z \sum_{j=1}^{N_{nei,i}} [\{W_{ij}^{*D} h_i\} - \{W_{ji}^{*D} h_j\}] - \Delta z \sum_{j=1}^{N_{nei,i}} W_{ij} \{h^*\} + A_i \Delta z \left\langle \frac{dP_i}{dt} \right\rangle$$



$$\frac{\Delta}{\Delta z} (\dot{m} h_i) = A_i \dot{q}_{eq,i} - \sum_{j=1}^{N_{nei,i}} W_{ij}^{*H} (h_j - h_i) - \sum_{j=1}^{N_{nei,i}} W_{ij} \{h^*\}$$

$$H_i^* \sum_{j=1}^{N_{nei,i}} W_{ij}$$

$$H_i^* = \frac{\sum_{j=1}^{N_{nei,i}} [ |x_{ij}| (h_i + h_j) - x_{ij} (h_i - h_j) ]}{2 \sum_{j=1}^{N_{nei,i}} |x_{ij}|}$$

$$W_{ij}^{*H} (h_i - h_j) = q''_{ij} s_{ij} \Big|_{conduction} + q''_{ij} s_{ij} \Big|_{turbulence}$$

$$q''_{ij} s_{ij} \Big|_{turbulence} = W_{ij}^{T,H} (h_i - h_j)$$

$$W_{ij}^{T,H} = \bar{\rho}_{ij} s_{ij} \left( \frac{\varepsilon_{ij}}{\eta_{ij}} \right)$$

- Boundary condition:  $T_{in}$

$$q''_{ij} s_{ij} \Big|_{conduction} = \bar{\rho}_{ij} s_{ij} \kappa_{ij} \left( \frac{\bar{\alpha}_{ij}}{\eta_{ij}} \right) (h_i - h_j) \quad \kappa \sim 1$$



# Physico-mathematical model: momentum conservation



Axial

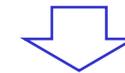
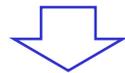
Radial

$$\Delta z \frac{\partial}{\partial t} \langle \dot{m}_i \rangle + \Delta [ \dot{m}_i \{ v_i \} ] = -A_i \Delta z \langle \rho_i \rangle g - A_i \Delta \{ P \}$$

$$- \Delta z \sum_{j=1}^{N_{nei}} [ \{ W_{ij}^{*D} v_i \} - \{ W_{ji}^{*D} v_j \} ] - \Delta z \sum_{j=1}^{N_{nei}} W_{ij} \{ v^* \}$$

$$- \Delta z \frac{1}{2} \langle \rho_i \rangle v_i^2 A_i \frac{f_i}{D_{H,i}} - A_i \Delta P_{form,i}$$

$$\frac{\partial}{\partial t} \langle W_{ij} \rangle + \frac{\Delta}{\Delta x'} [ W_{ij} \{ u \} ] + \frac{\Delta}{\Delta z} [ W_{ij} \{ v \} ] = - \left[ s_{ij} \frac{\Delta}{\Delta x} \{ P_j \} \right] - \left\{ \frac{F_{ix}}{\Delta x' \Delta z} \right\}$$



$$\frac{\Delta (\dot{m}_i v_i)}{\Delta z} = -A_i \langle \rho_i \rangle g - A_i \frac{\Delta \{ P \}}{\Delta z}$$

$$- \sum_{j=1}^{N_{nei}} W_{ij}^{*M} (v_i - v_j) - \sum_{j=1}^{N_{nei}} W_{ij} \{ v^* \}$$

$$- \frac{1}{2} \langle \rho_i \rangle v_i^2 A_i \frac{f_i}{D_{H,i}} - A_i \frac{\Delta P_{form,i}}{\Delta z}$$

$$P_i = P_j \quad \forall i, j$$

- Boundary condition:  $p_{in}$

- Implemented empirical correlations for  $f$ :
  - Turbulent: Blasius, Colebrook, Haaland
  - Laminar: Liang

With correction factor for non-circular geometries from Idelchick handbook



# Physico-mathematical model: flow split and heat transfer to wrapper



## Flow split

$$v_i^2 \frac{f_i}{D_{H,i}} L + \xi_i v_i^2 = v_j^2 \frac{f_j}{D_{H,j}} L + \xi_j v_j^2$$

$$\begin{bmatrix} 1 & -K_{21} & 0 & \dots & 0 & 0 \\ 0 & 1 & -K_{32} & & 0 & 0 \\ \vdots & & & \ddots & & \vdots \\ 0 & 0 & 0 & & 1 & -K_{N_{cat} N_{cat}-1} \\ \frac{N_1 A_1}{A_{tot}} & \frac{N_2 A_2}{A_{tot}} & \frac{N_3 A_3}{A_{tot}} & \dots & \frac{N_{N_{cat}-1} A_{N_{cat}-1}}{A_{tot}} & \frac{N_{N_{cat}} A_{N_{cat}}}{A_{tot}} \end{bmatrix} \begin{bmatrix} X_1 \\ X_2 \\ \vdots \\ X_{N_{cat}-1} \\ X_{N_{cat}} \end{bmatrix} = \begin{bmatrix} 0 \\ 0 \\ \vdots \\ 0 \\ 1 \end{bmatrix}$$

## Heat transfer to wrapper

$$T_{w,o,m} = T_{sc} + q''_{w,o,m} / \alpha_o$$

$$T_{w,i,m} = T_{w,o,m} + \frac{q''_{w,o,m} k_w}{s_w}$$

- Implemented empirical correlations for  $Nu$ :
  - Kays, Duchatelle, Dwyer, Sleicher/Rouse, Paradis



# Data modelling



- Identify the needed input and output quantities, based on:
  - Requirements stated in the SRS
  - Specific needs of the selected problem-solving approach
- Identify the quantities to be treated by the code
  - Based on the selected problem-solving approach
  - Include user inputs to modify code behavior as needed

| Numerics  |                     |                                                     |       |
|-----------|---------------------|-----------------------------------------------------|-------|
| Column    | Data type           | Description                                         | Notes |
| nAxNod    | int                 | Number of axial nodes                               |       |
| zAxNod    | float<br>(nAxNod+1) | Axial coordinates of node boundaries                |       |
| cRadDiscr | string              | Label identifying the selected approach for the ra- |       |

| Materials |           |                                                                |                                       |
|-----------|-----------|----------------------------------------------------------------|---------------------------------------|
| Column    | Data type | Description                                                    | Notes                                 |
| cLm       | string    | Label identifying the coolant type                             | in case = 'default'. ch SA            |
| cWrap     | string    | Label identifying the wrapper material                         | in case = 'manual', defined radial on |
| cLmDens   | string    | Label identifying the selected correlation for coolant density | in case = 'manual'                    |

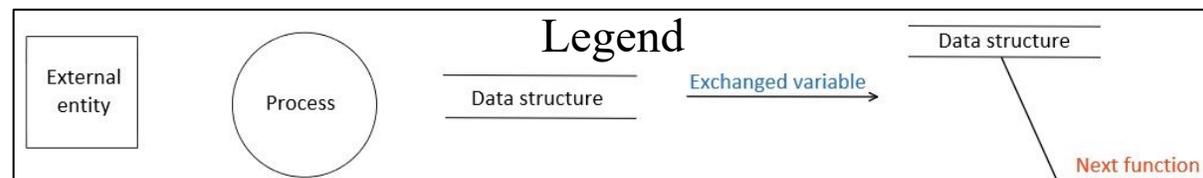
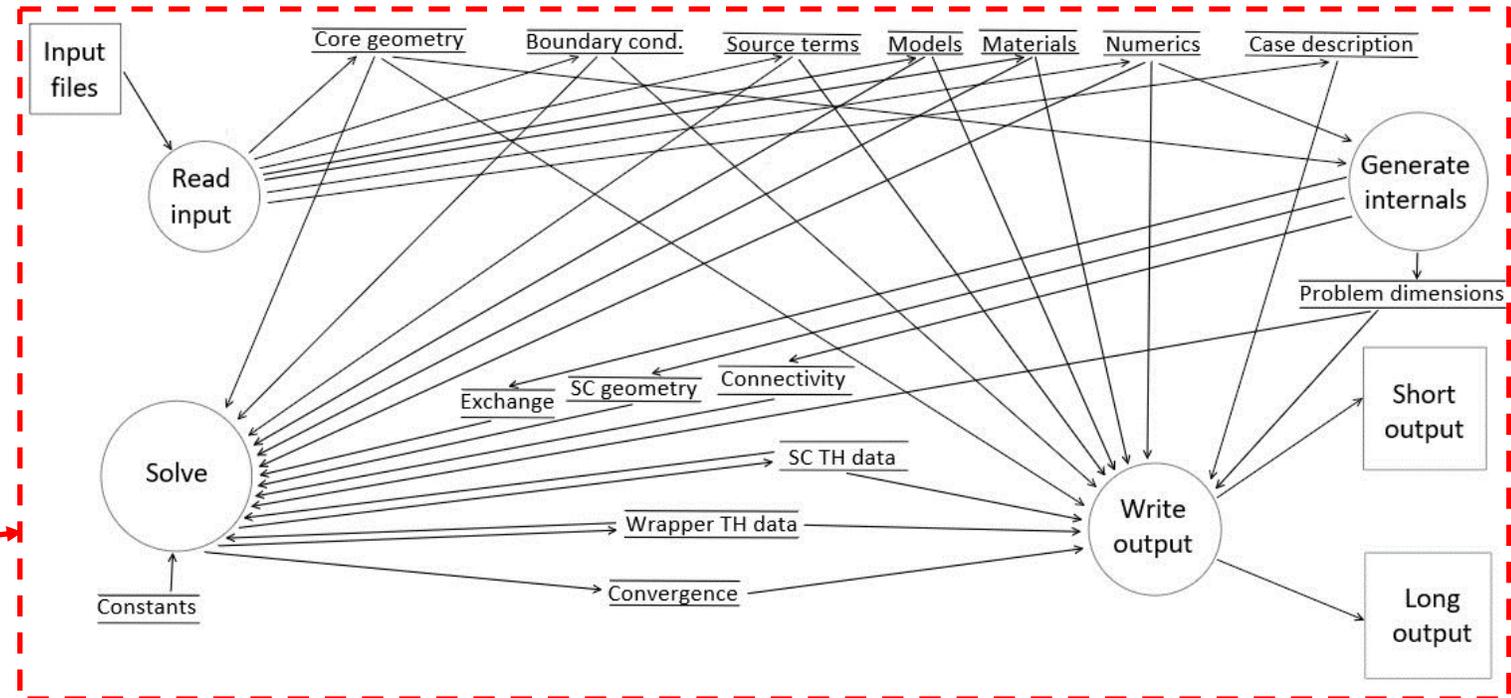
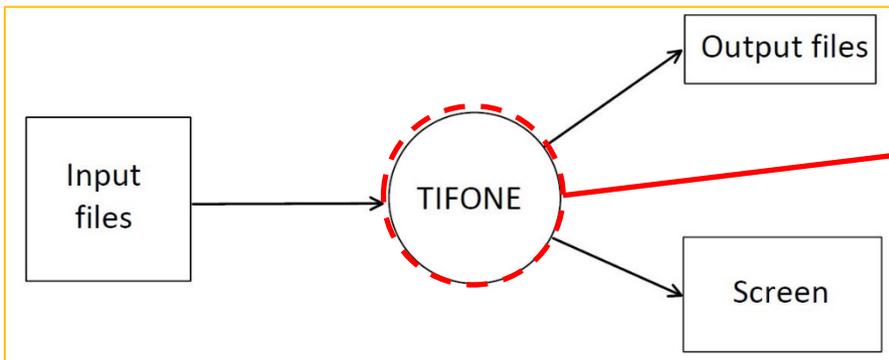
| SC TH data |                    |                 |       |
|------------|--------------------|-----------------|-------|
| Column     | Data type          | Description     | Notes |
| temp       | float(nSc, nAxNod) | Temperature     |       |
| velc       | float(nSc, nAxNod) | Flow velocity   |       |
| dens       | float(nSc, nAxNod) | Coolant density |       |
| enth       | float(nSc, nAxNod) | Enthalpy        |       |

| Boundary conditions |           |                                                              |                                                                                        |
|---------------------|-----------|--------------------------------------------------------------|----------------------------------------------------------------------------------------|
| Column              | Data type | Description                                                  | Notes                                                                                  |
| tempInlet           | float     | Core inlet temperature                                       |                                                                                        |
| mdotIn              | float     | Total core mass flow rate                                    |                                                                                        |
| iwFrac              | float     | Fraction of the core mass flow rate flowing in the IW region | The IW flow rate is then distributed among the SCs based on the flow split calculation |
| presInlet           | float     | Core inlet pressure                                          | Defaults to 0.0 Pa                                                                     |

# Functional modelling (I)



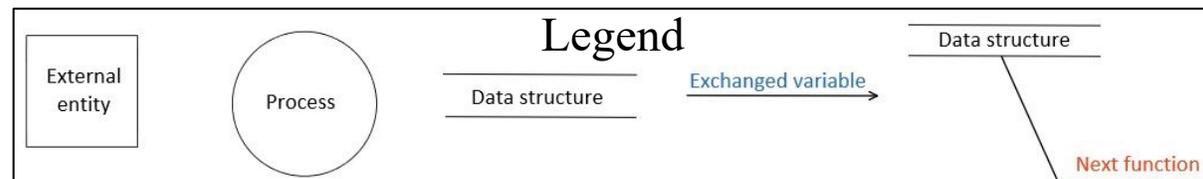
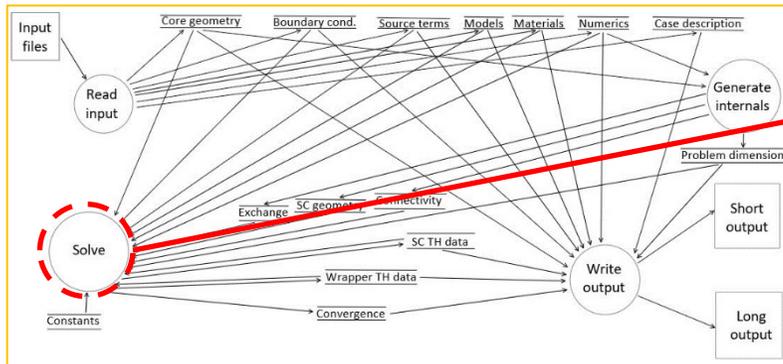
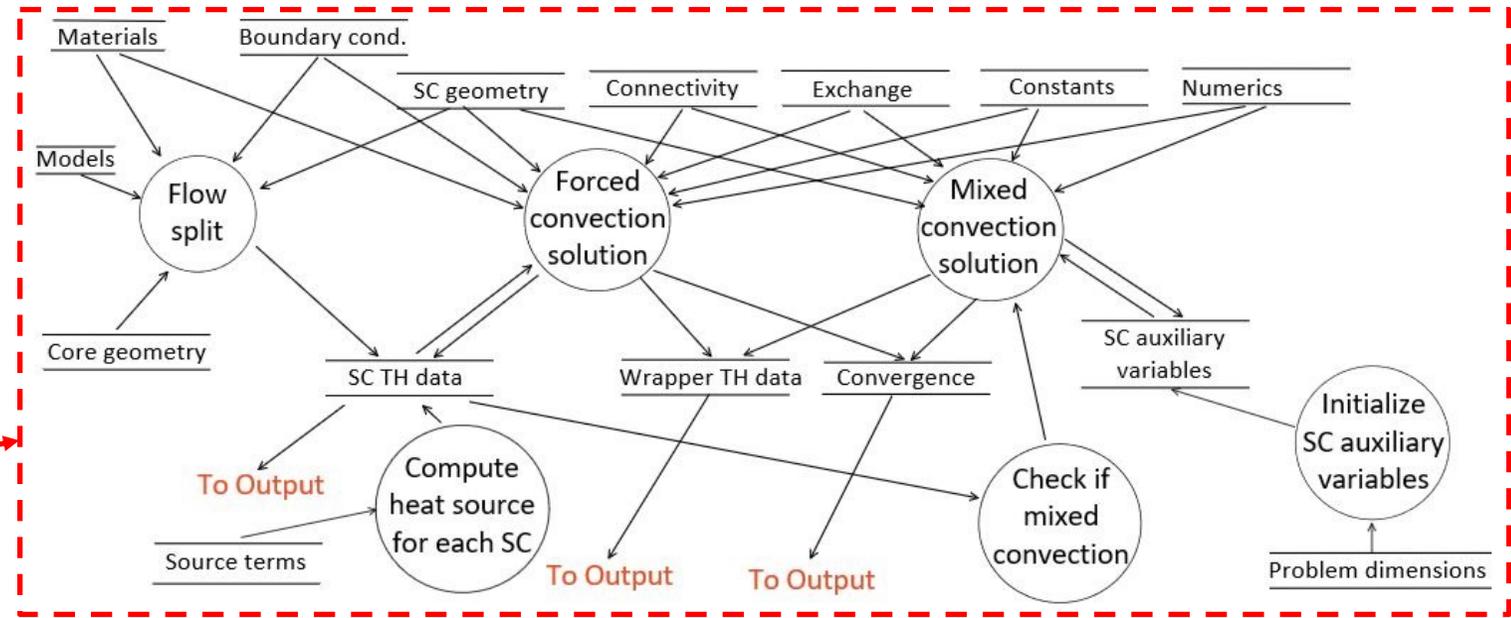
- Aim: identify the transformations undergone by data contained in data structures.
- Increase level of detail until functions are highly *consistent*
- Graphical representation: DFDs



# Functional modelling (II)



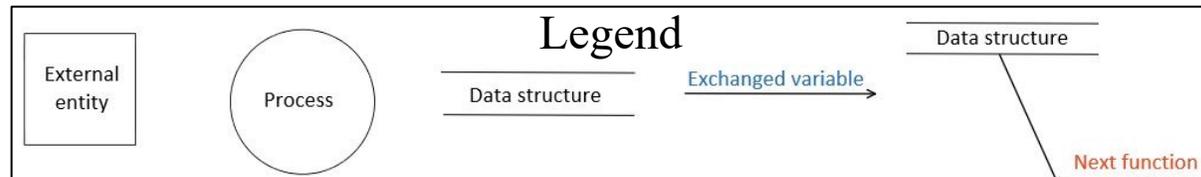
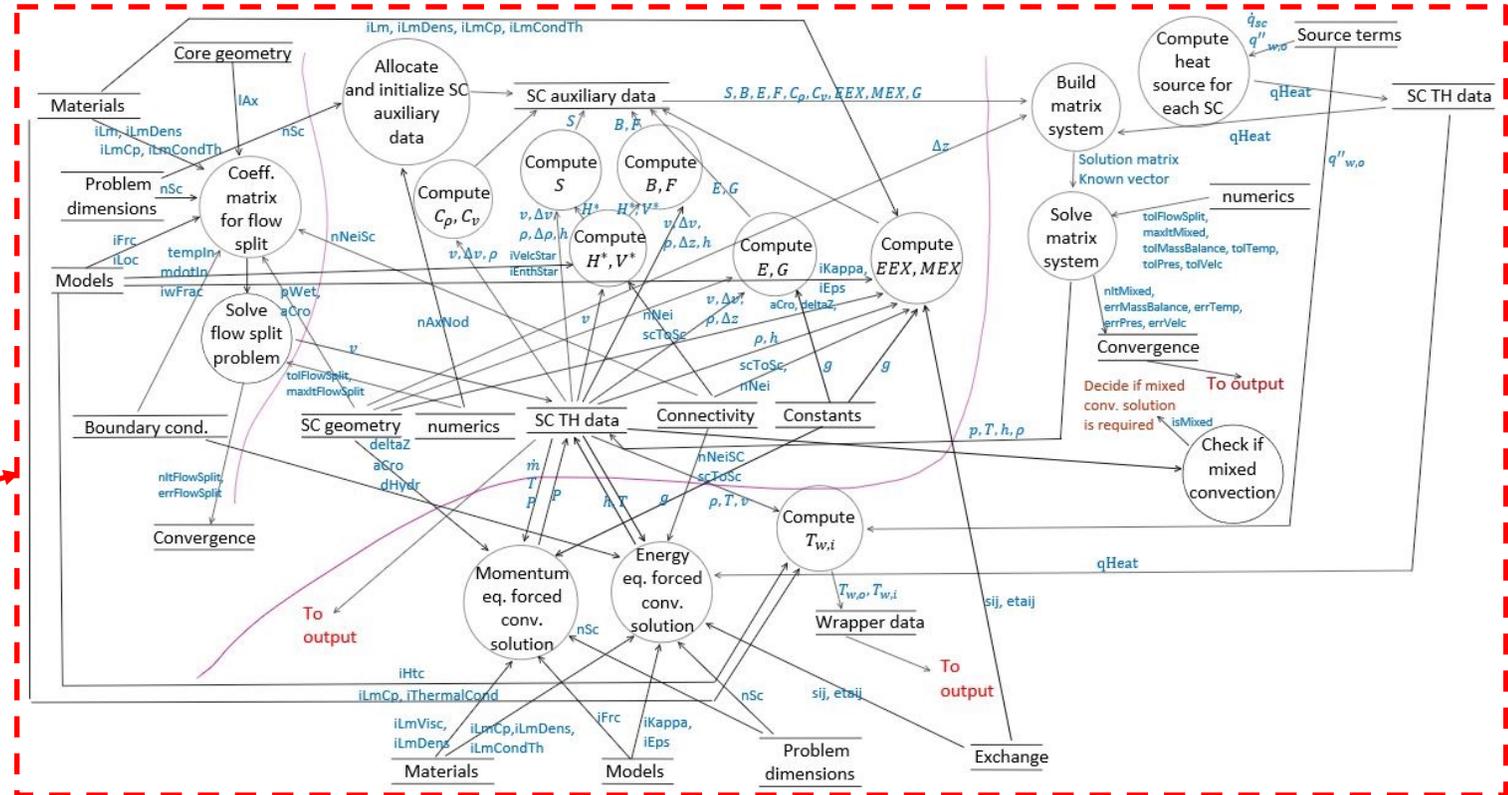
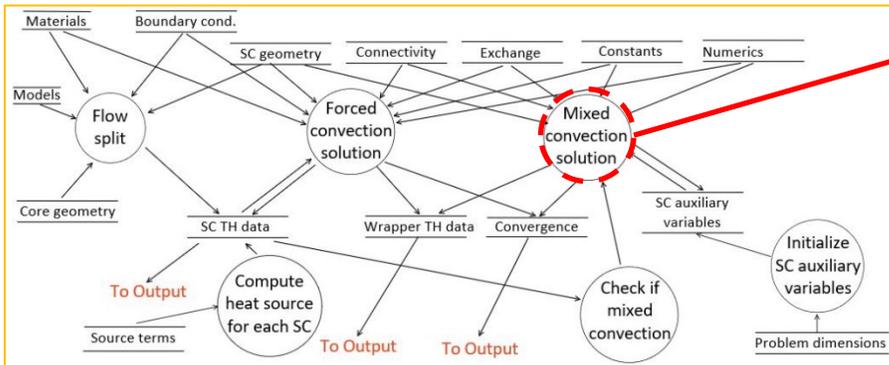
- Aim: identify the transformations undergone by data contained in data structures.
- Increase level of detail until functions are highly *consistent*
- Graphical representation: DFDs



# Functional modelling (III)



- Aim: identify the transformations undergone by data contained in data structures.
- Increase level of detail until functions are highly *consistent*
- Graphical representation: DFDs

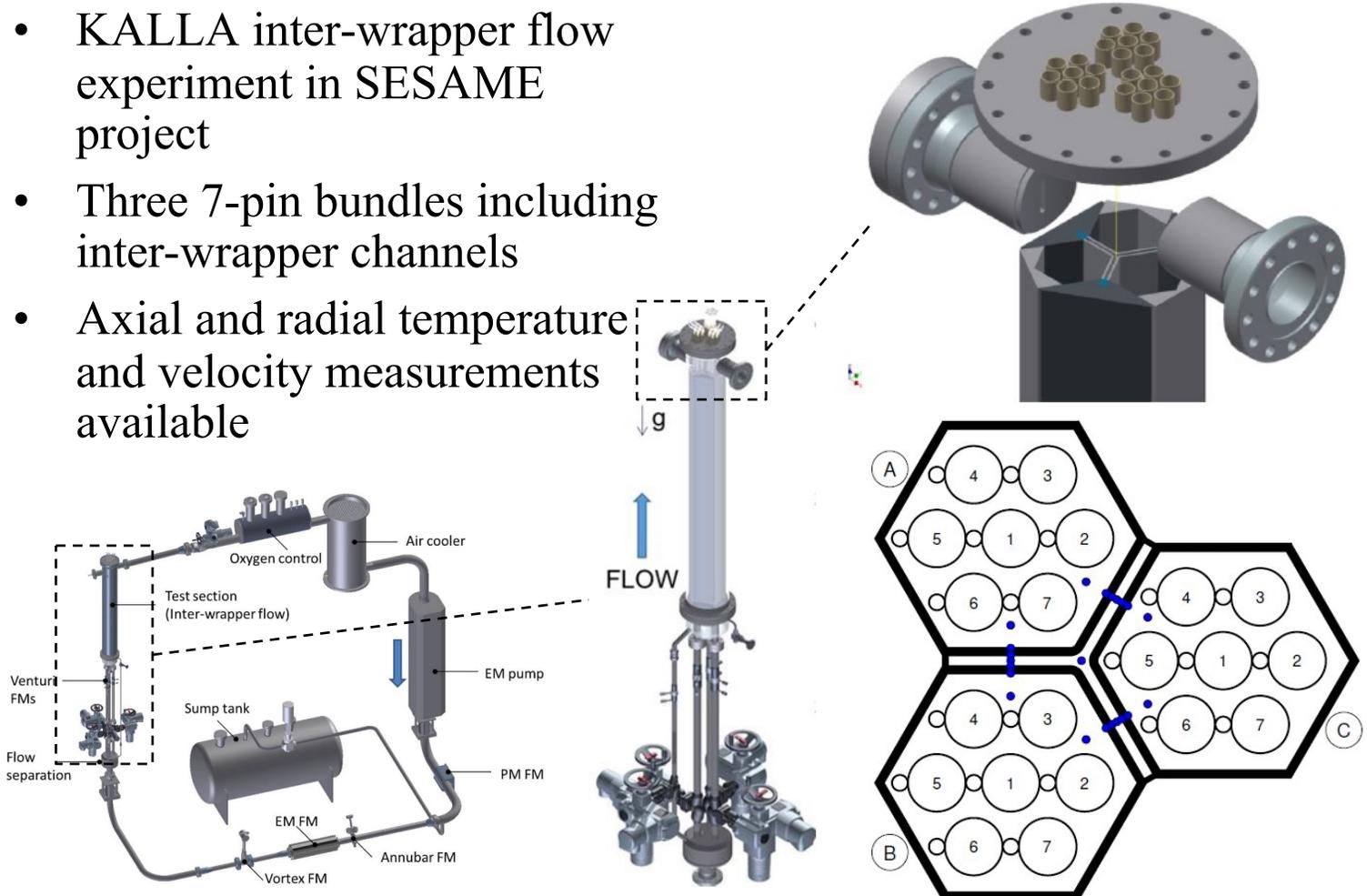


# KALLA IW flow experiments



| Quantity                   | Unit            | Value  | Meaning                      |
|----------------------------|-----------------|--------|------------------------------|
| <b>Outer dimensions</b>    |                 |        |                              |
| $FF$                       | mm              | 65.00  | Outer flat-to-flat distance  |
| $w$                        | mm              | 2.0    | Wall thickness               |
| $\delta$                   | mm              | 3.0    | Gap width                    |
| <b>Bundle dimensions</b>   |                 |        |                              |
| $D$                        | mm              | 16.0   | Rod diameter                 |
| $L_{heat}$                 | mm              | 600.0  | Rod heated length            |
| $L_{tot}$                  | mm              | 1400.0 | Rod total length             |
| $P$                        | mm              | 20.50  | Rod pitch                    |
| $d$                        | mm              | 4.40   | Wire diameter                |
| $H$                        | mm              | 262.0  | Wire pitch                   |
| $W$                        | mm              | 20.75  | Wall distance                |
| <b>Ratios</b>              |                 |        |                              |
| $P/D$                      | -               | 1.281  | Pitch-to-diameter            |
| $H/D$                      | -               | 16.375 | Wire pitch-to-diameter       |
| $W/D$                      | -               | 1.297  | Wall-distance-to-diameter    |
| <b>Flow areas</b>          |                 |        |                              |
| $A_{bd}$                   | mm <sup>2</sup> | 1704.2 | Bundle channels (A-C)        |
| $A_{int}$                  | mm <sup>2</sup> | 73.6   | Bundle internal sub-channels |
| $A_{edge}$                 | mm <sup>2</sup> | 152.9  | Bundle edge sub-channels     |
| $A_{corner}$               | mm <sup>2</sup> | 57.5   | Bundle internal sub-channels |
| $A_{gap}$                  | mm <sup>2</sup> | 331.9  | Gap channel (D)              |
| <b>Hydraulic diameters</b> |                 |        |                              |
| $d_{h,bdl}$                | mm              | 10.31  | Bundle channels (A-C)        |
| $d_{h,int}$                | mm              | 9.1    | Bundle internal sub-channels |
| $d_{h,edge}$               | mm              | 11.6   | Bundle edge sub-channels     |
| $d_{h,corner}$             | mm              | 9.1    | Bundle internal sub-channels |
| $d_{h,gap}$                | mm              | 5.85   | Gap channel (D)              |

- KALLA inter-wrapper flow experiment in SESAME project
- Three 7-pin bundles including inter-wrapper channels
- Axial and radial temperature and velocity measurements available



# Overview on validation dataset



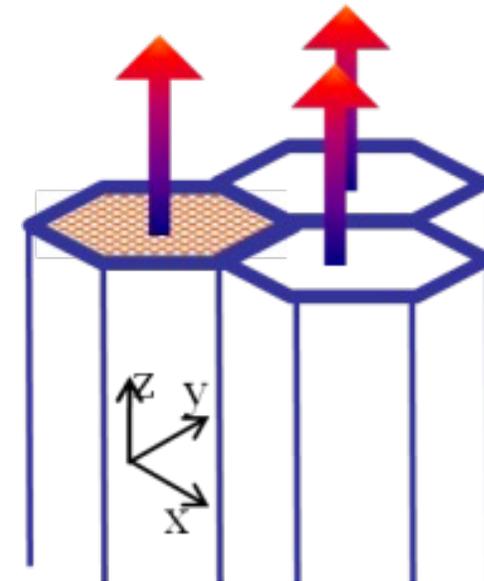
- Both **symmetric** and **asymmetric** cases performed
- Flow conditions: laminar/turbulent
- Heat flux boundary conditions: from **three standalone ANTEO+runs** (one for each FA) with total power to IW rescaled to match measured power
- Mixed convection solution

Nominal conditions:

| Quantity  | Unit              | Value  | Meaning                | Notes       |
|-----------|-------------------|--------|------------------------|-------------|
| $\dot{m}$ | kg/s              | 0.686  | Inlet mass flow rate   |             |
| $T_{in}$  | °C                | 199.25 | Inlet LBE temperature  |             |
| $q_{tot}$ | kW                | 3.700  | Total power to IW flow |             |
| $q''$     | kW/m <sup>2</sup> | $f(z)$ | Surface heat flux      | From ANTEO+ |

*Note: the code can simulate also other LMs (e.g. Na), therefore other validation cases considering these fluids can be considered in the future.*

Acknowledgement: access to SESAME dataset courtesy of Dr. M. Tarantino, access to full dataset courtesy of Dr. J. Pacio.





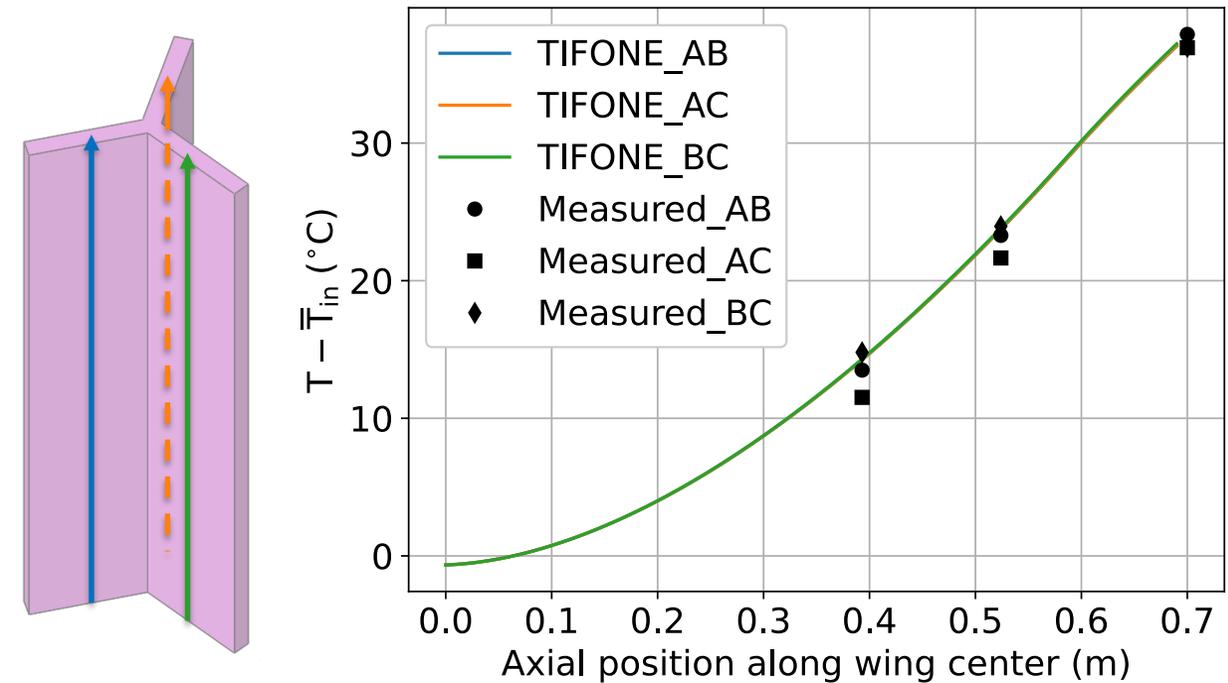
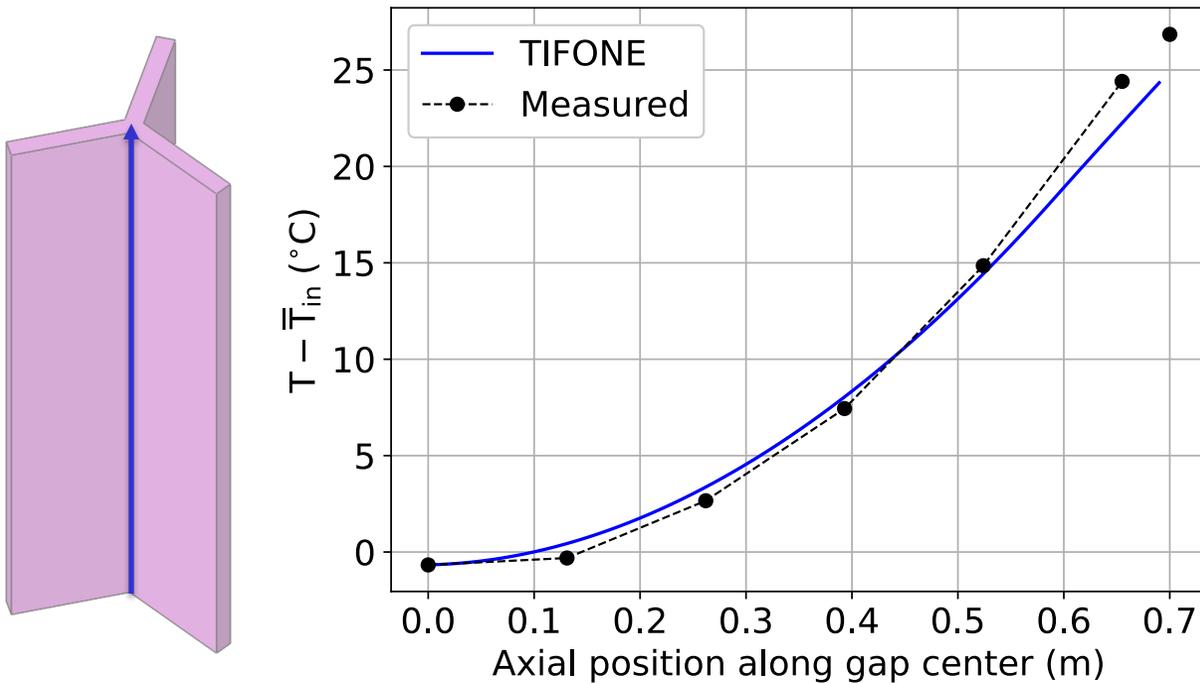
# Symmetric validation cases

| Quantity                                  | Unit | Case 1       | Case 3       | Case 6       | Case 8      |
|-------------------------------------------|------|--------------|--------------|--------------|-------------|
| $\dot{m}$ – IW mass flow rate             | kg/s | <b>0.686</b> | <b>0.517</b> | <b>0.342</b> | <b>0.17</b> |
| $\dot{m}_A \sim \dot{m}_B \sim \dot{m}_C$ | kg/s | 3.55         | 3.55         | 3.55         | 3.55        |
| $q_{tot}$ – Total power to IW flux        | kW   | 3.700        | 3.010        | 2.160        | 1.170       |
| $q_A \sim q_B \sim q_C$                   | kW   | 30.00        | 30.00        | 30.00        | 30.00       |
| $T_{in}$ – Inlet LBE temperature          | °C   | 199.25       | 199.20       | 199.10       | 199.10      |

*Note: here and thereafter, uncertainties on measured quantities are not indicated for the sake of clarity*

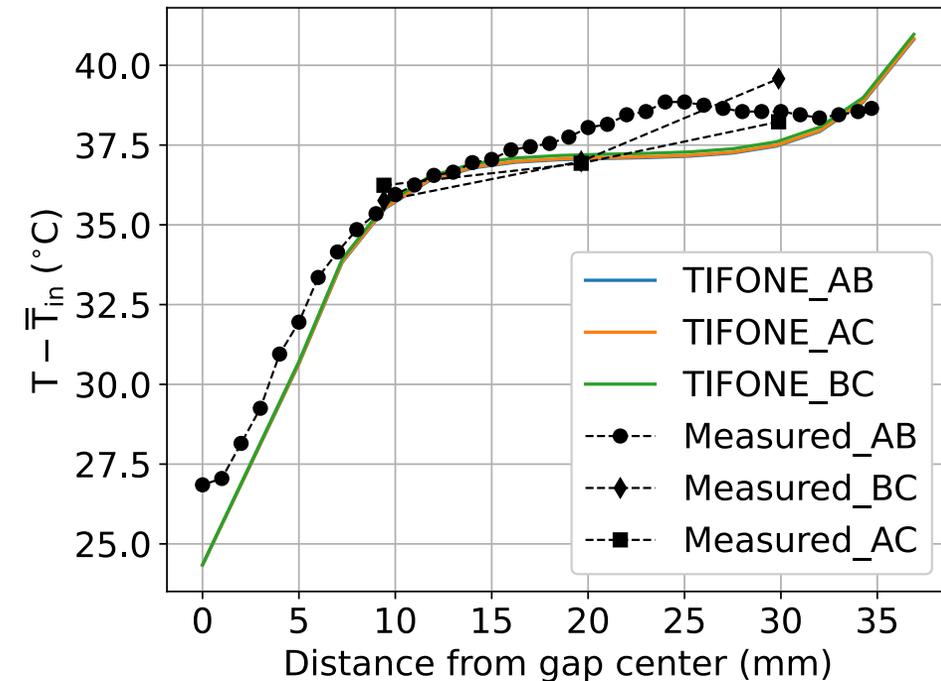
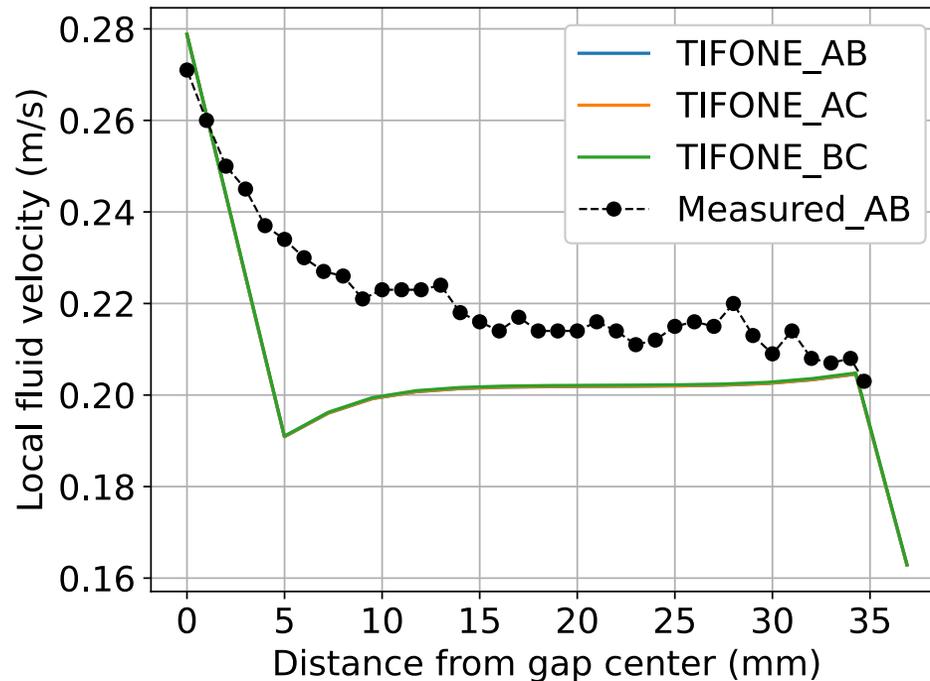
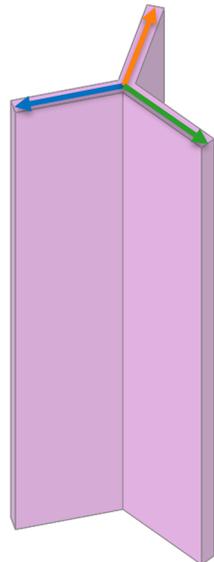


# Symmetric case #1: axial temperature profiles



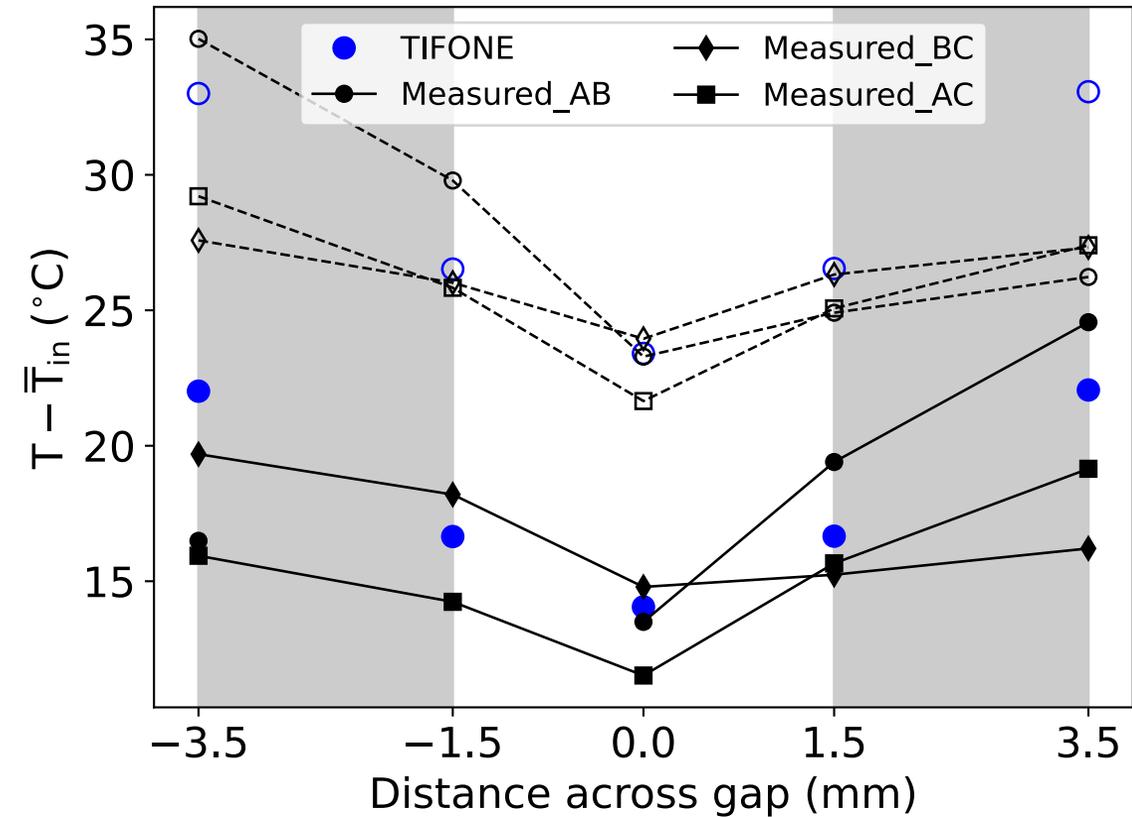
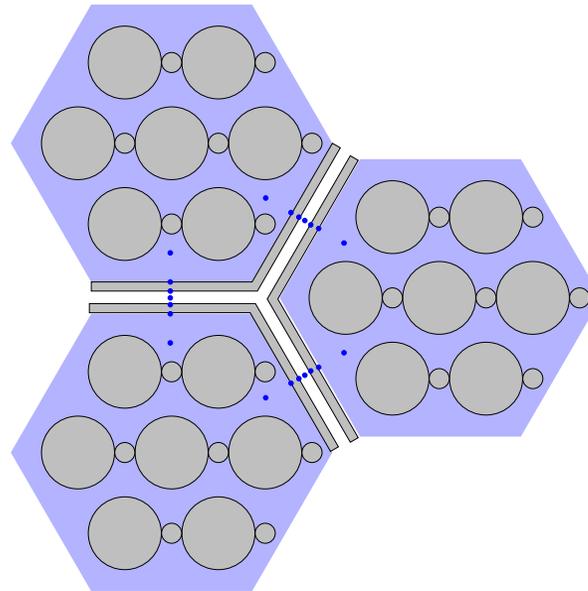
# Symmetric case #1: radial temperature profiles

- Satisfactory agreement on velocity profile
  - To be assessed: local measurements, but averaged quantities per SC computed
- Very good agreement on radial coolant temperature distribution
- To be confirmed by considering a case with larger number of SAs

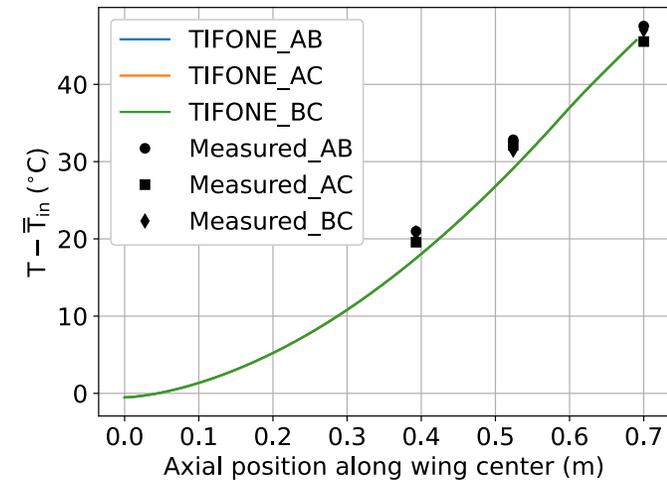
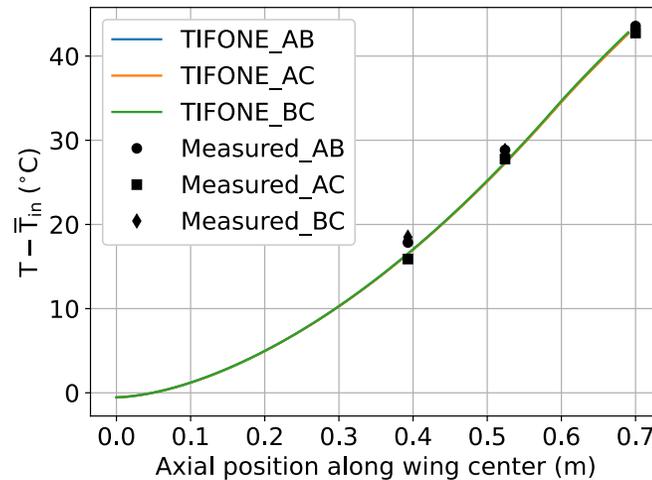
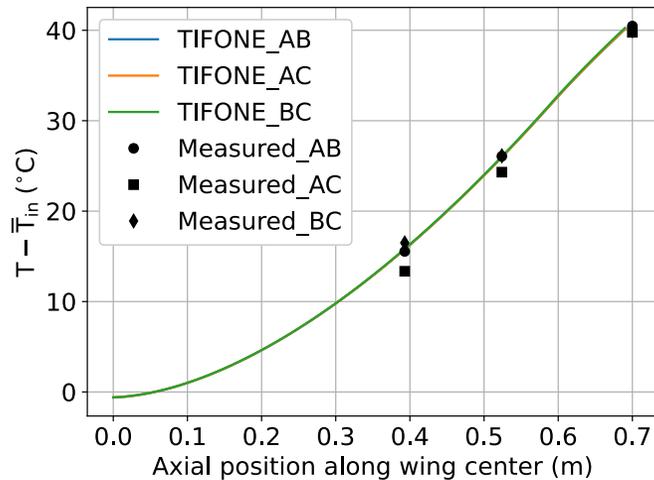
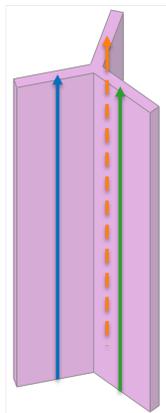
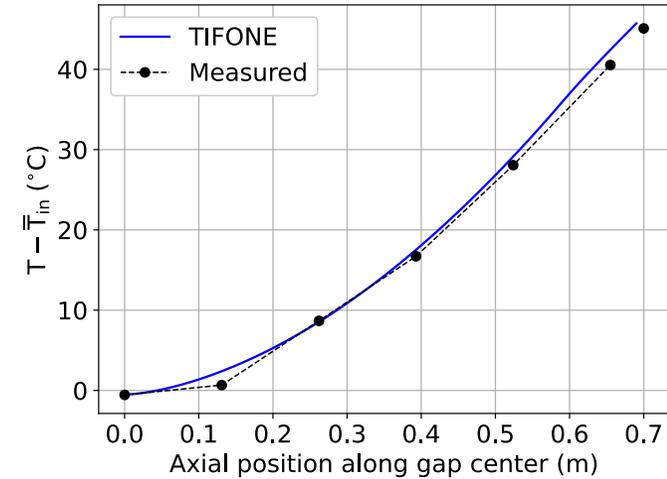
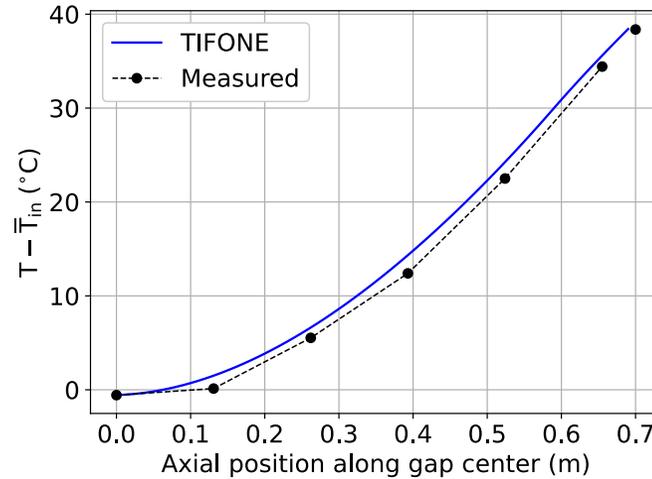
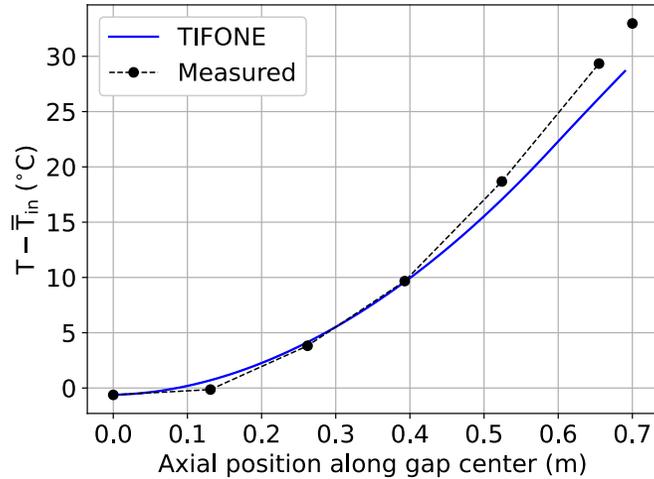
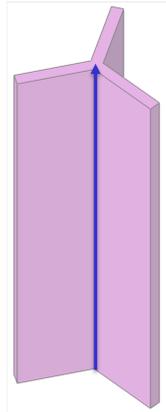




# Symmetric case #1: wrapper temperatures



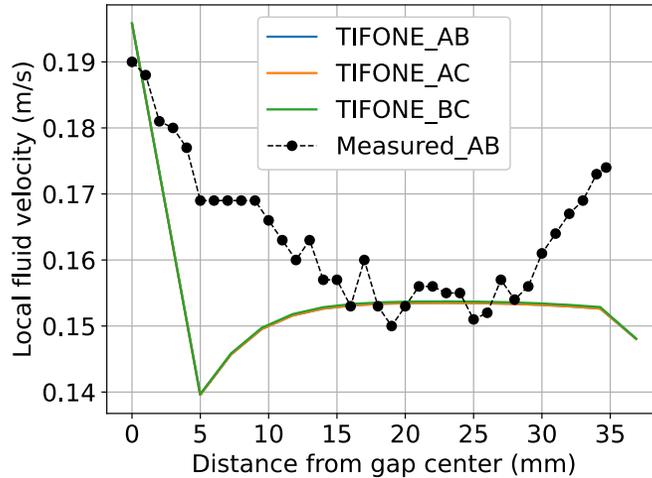
# Symmetric cases #3,6,8: axial temperature profiles



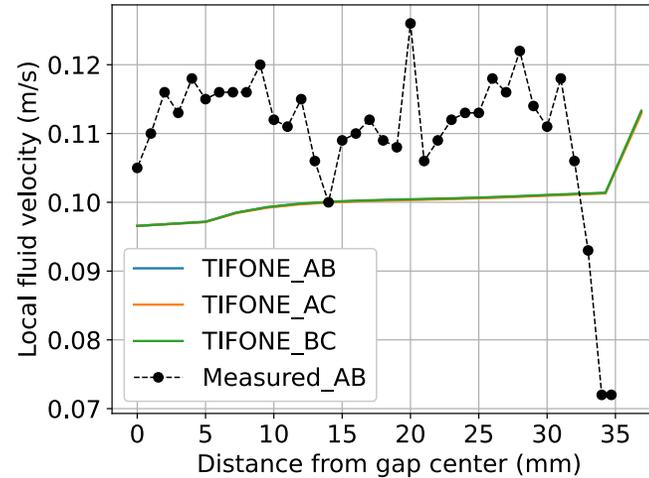
# Symmetric cases #3,6,8: radial velocity and temperature profiles

$\dot{m}_{IW}$  reduced

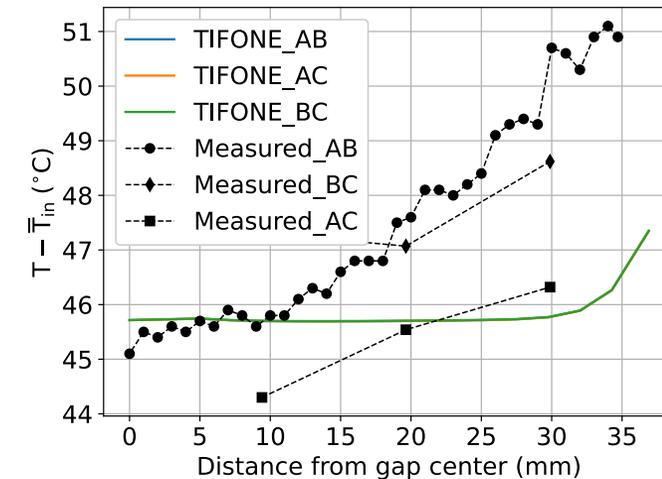
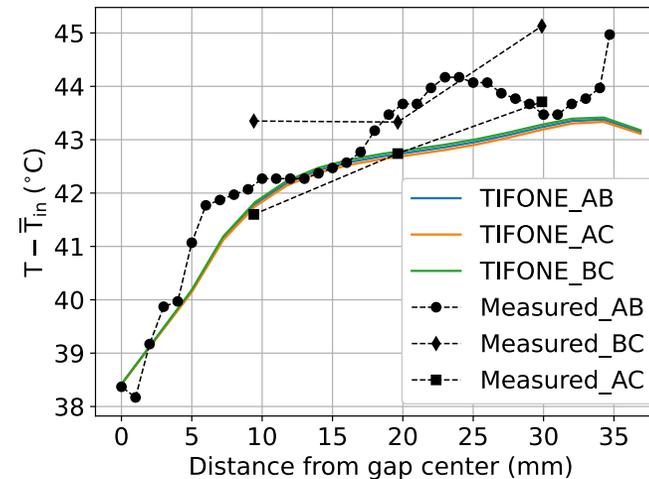
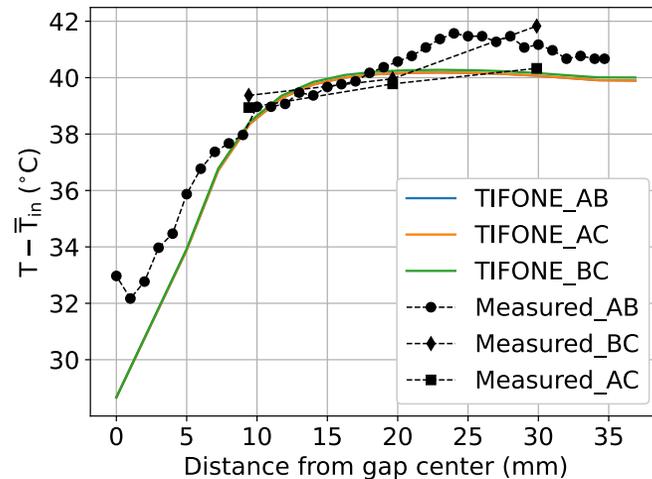
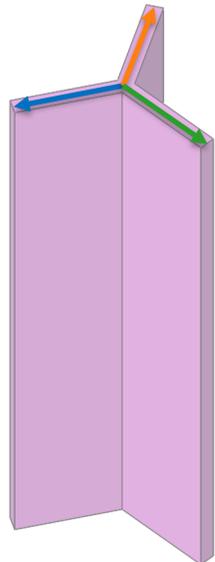
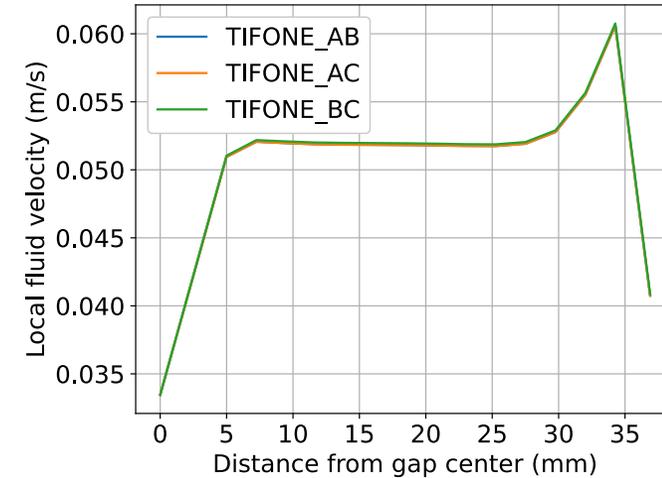
#3:  $Y_{mix} = 0.0031$



#6:  $Y_{mix} = 0.0045$



#8:  $Y_{mix} = 0.0087$



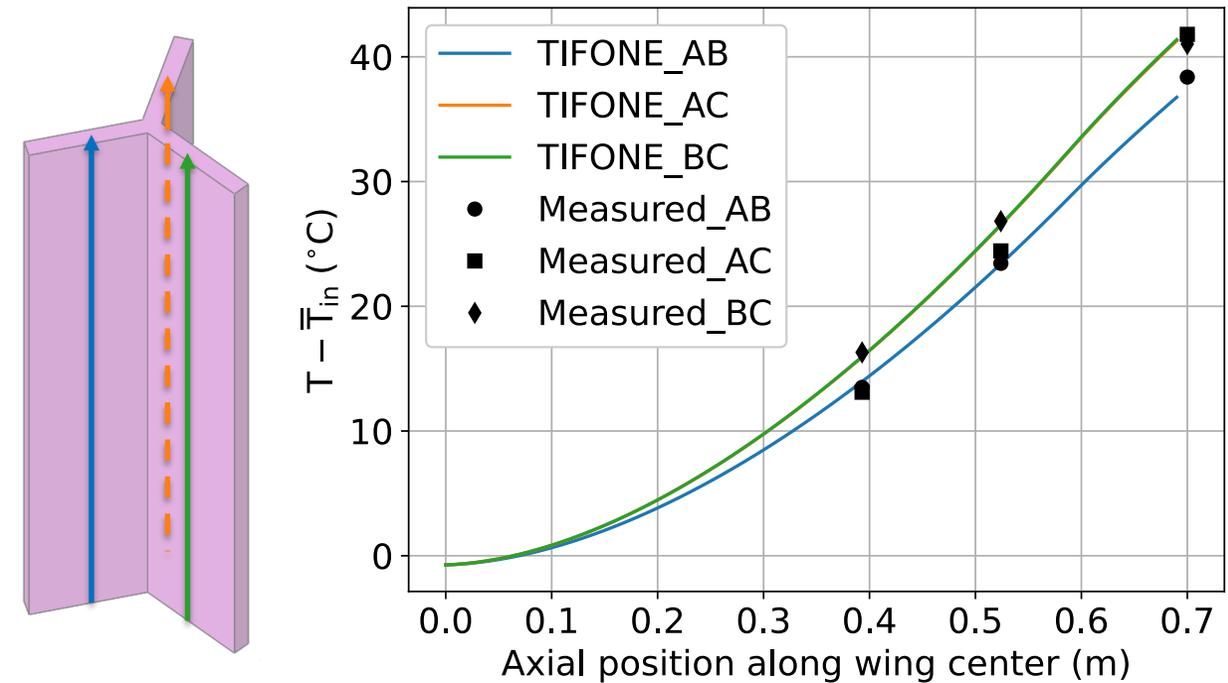
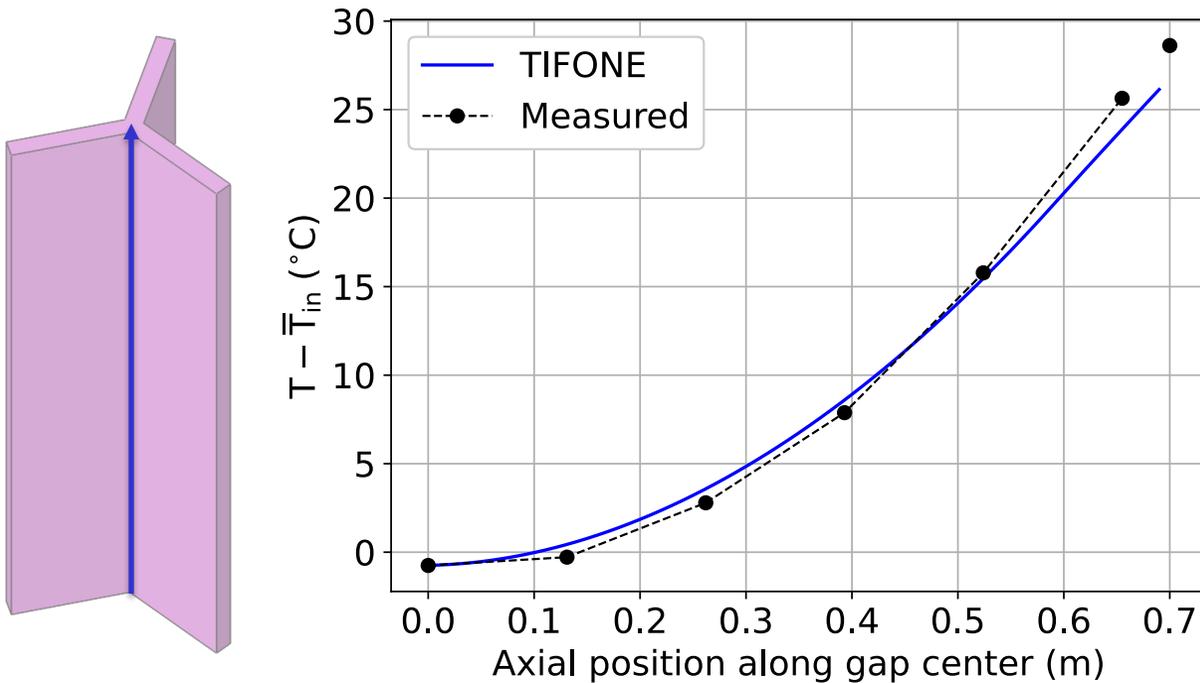


# Aymmetric validation cases: reduced flow rate in C by 20%

| Quantity                           | Unit | Case 1       | Case 3       | Case 6       | Case 8      |
|------------------------------------|------|--------------|--------------|--------------|-------------|
| $\dot{m}$ – IW mass flow rate      | kg/s | <b>0.686</b> | <b>0.517</b> | <b>0.342</b> | <b>0.17</b> |
| $\dot{m}_A \sim \dot{m}_B$         | kg/s | 3.55         | 3.55         | 3.55         | 3.55        |
| $\dot{m}_C$                        | kg/s | <b>2.86</b>  | <b>2.86</b>  | <b>2.86</b>  | <b>2.86</b> |
| $q_{tot}$ – Total power to IW flux | kW   | 3.700        | 3.010        | 2.160        | 1.170       |
| $q_A \sim q_B \sim q_C$            | kW   | 30.00        | 30.00        | 30.00        | 30.00       |
| $T_{in}$ – Inlet LBE temperature   | °C   | 199.25       | 199.20       | 199.10       | 199.10      |

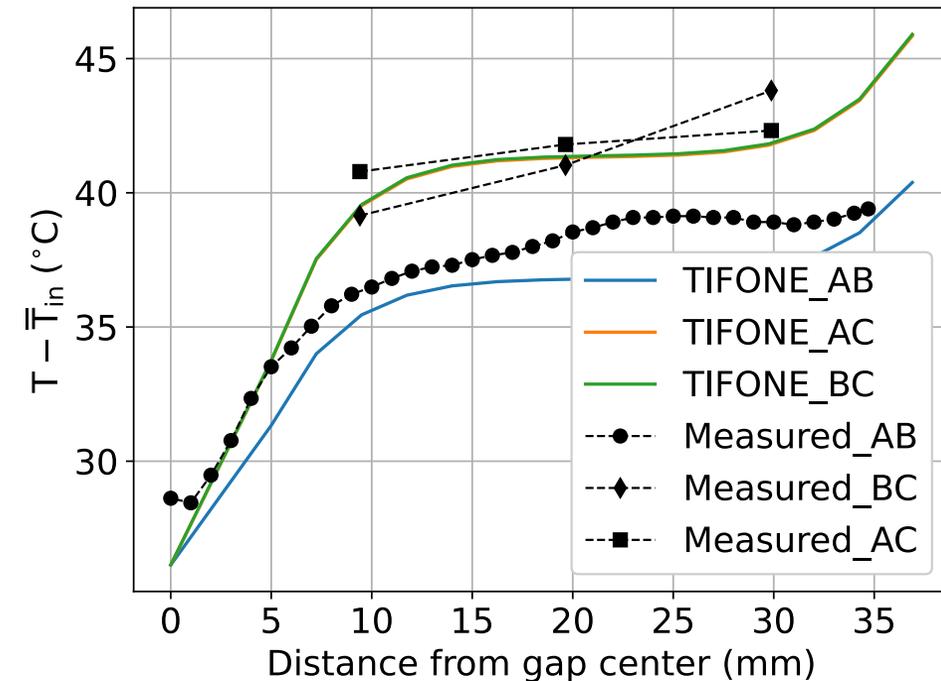
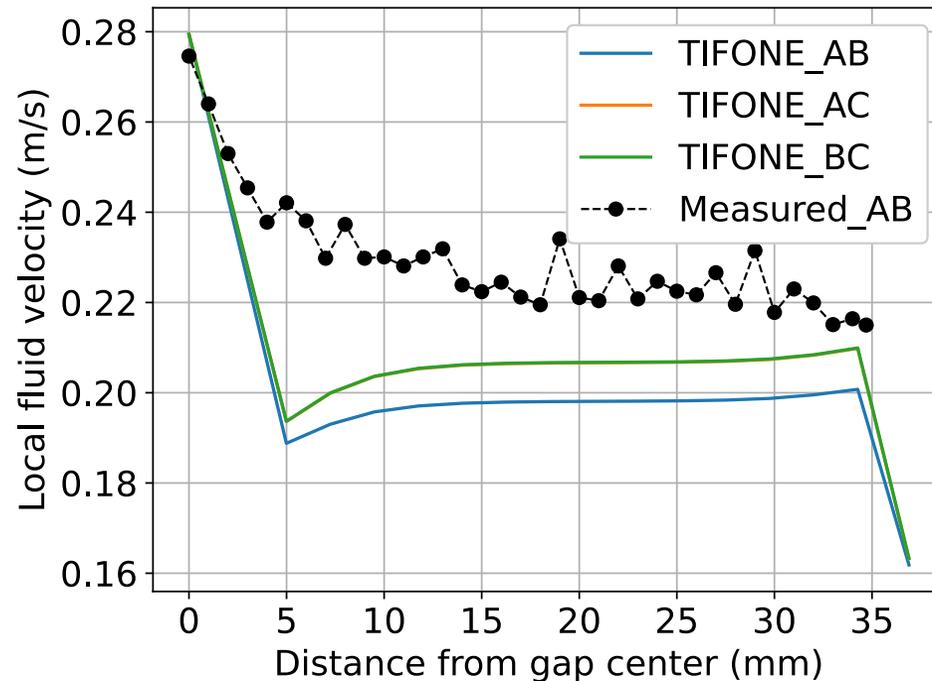
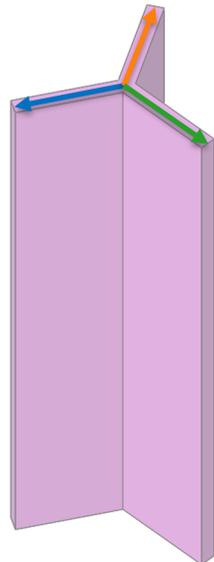


# Asymmetric case #42: axial temperature profiles



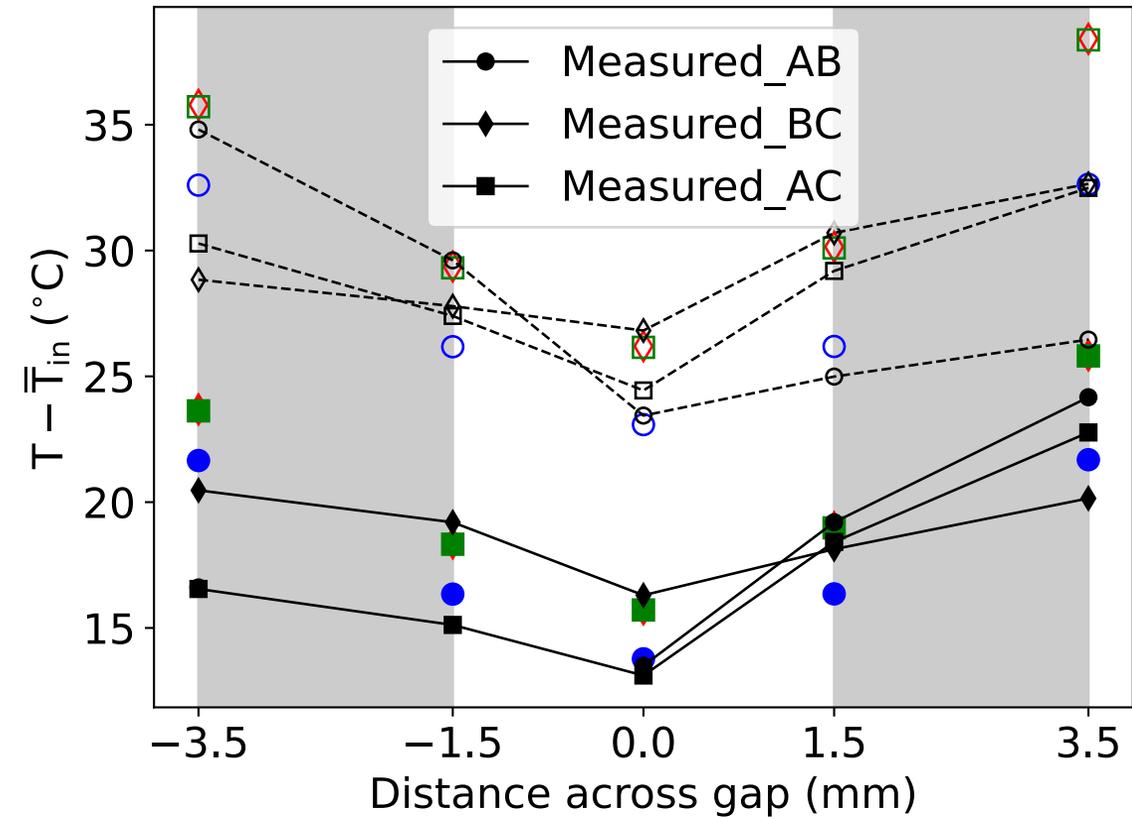
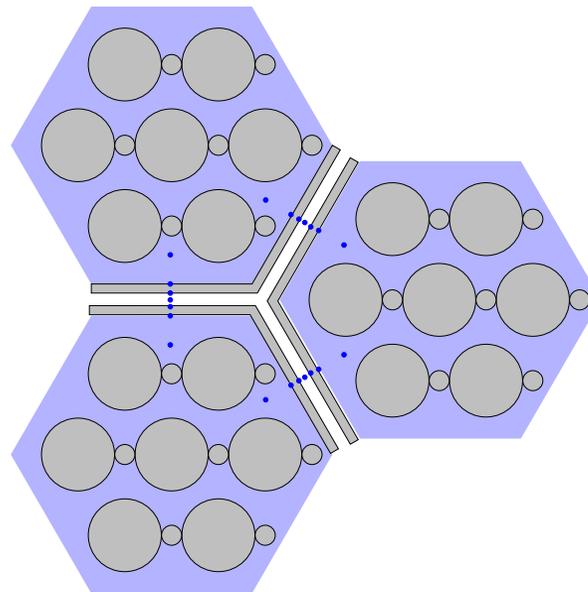
# Asymmetric case #42: radial temperature profiles

- Satisfactory agreement on velocity profile
  - To be assessed: local measurements, but averaged quantities per SC computed
- Very good agreement on radial coolant temperature distribution
- To be confirmed by considering a case with larger number of SAs

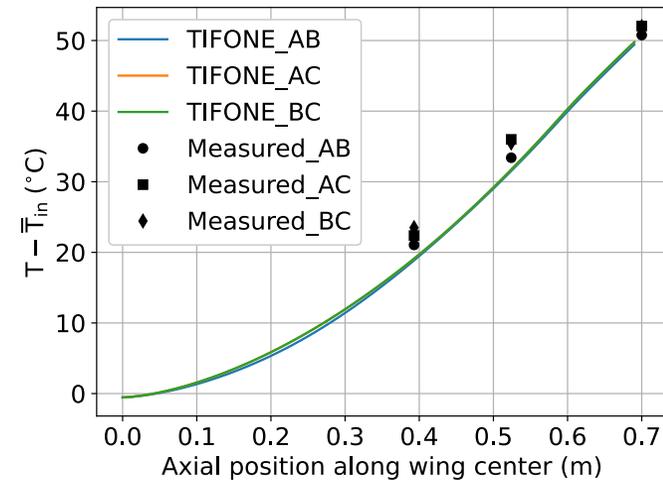
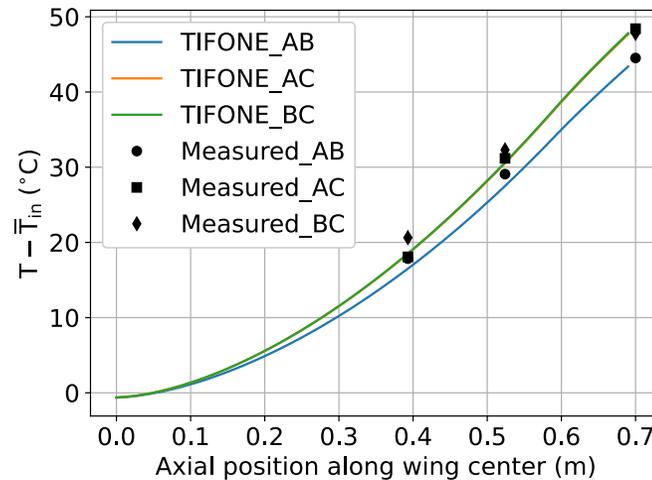
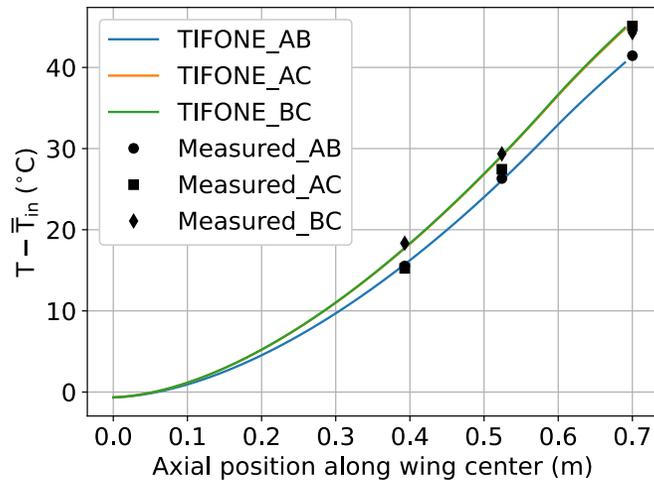
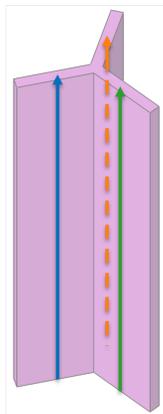
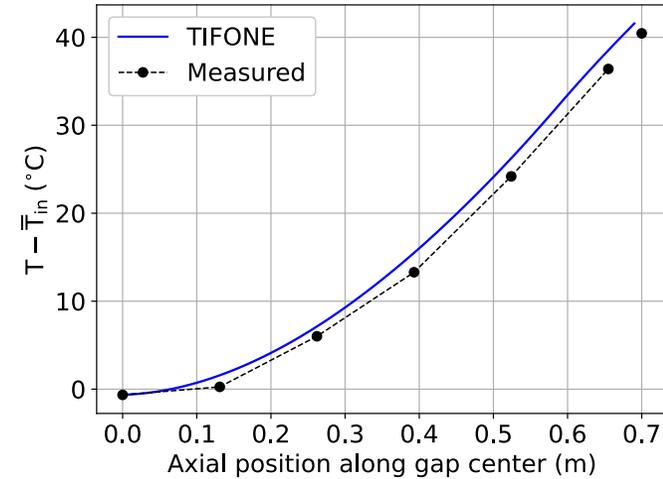
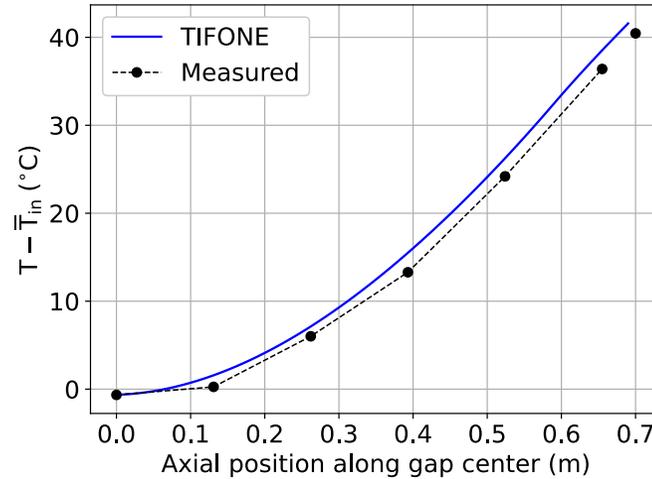
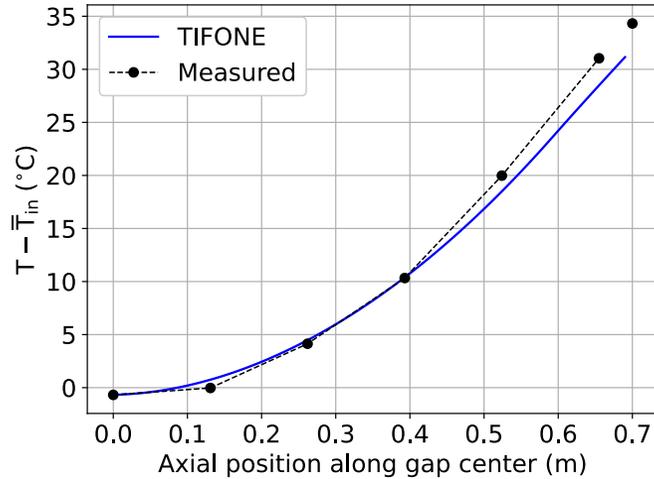
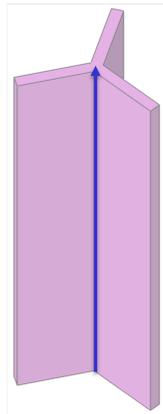




# Asymmetric case #42: wrapper temperatures



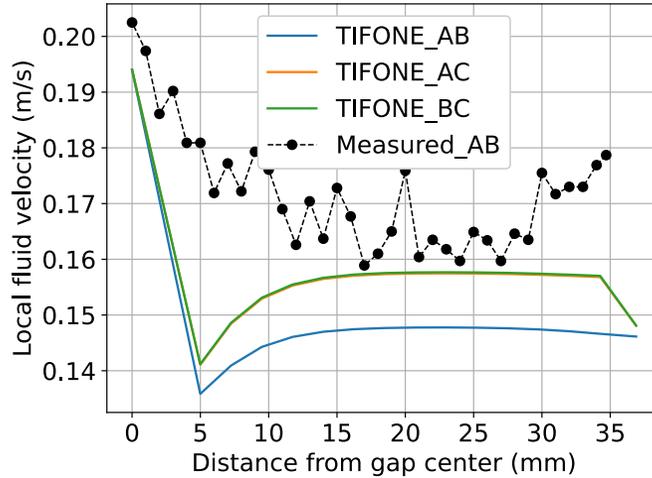
# Asymmetric cases # 45,48,51: axial temperature profiles



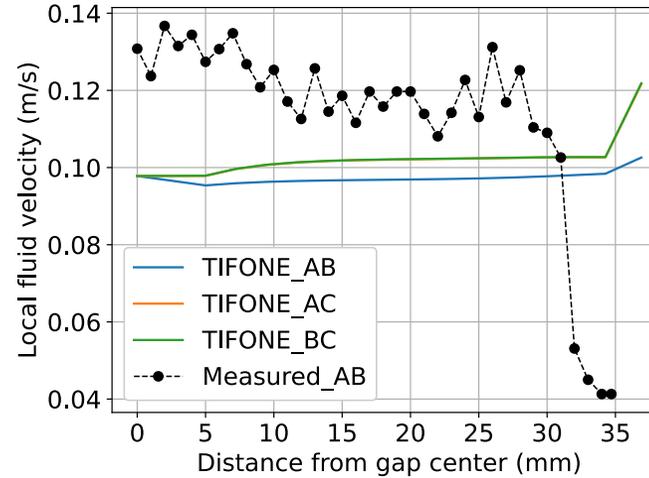
# Asymmetric cases # 45,48,51: axial temperature profiles

$\dot{m}_{IW}$  reduced

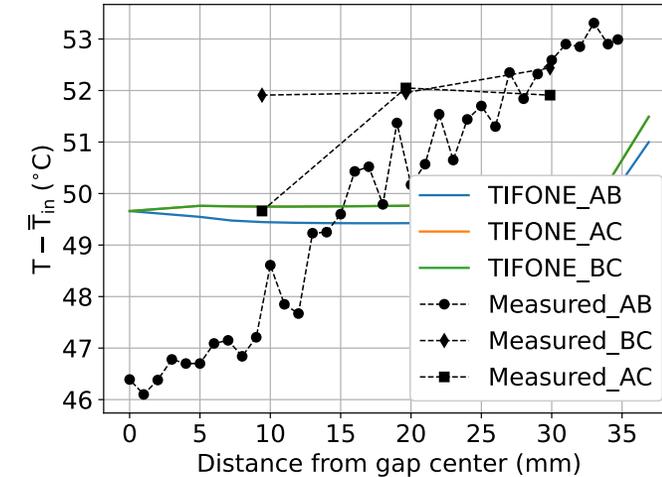
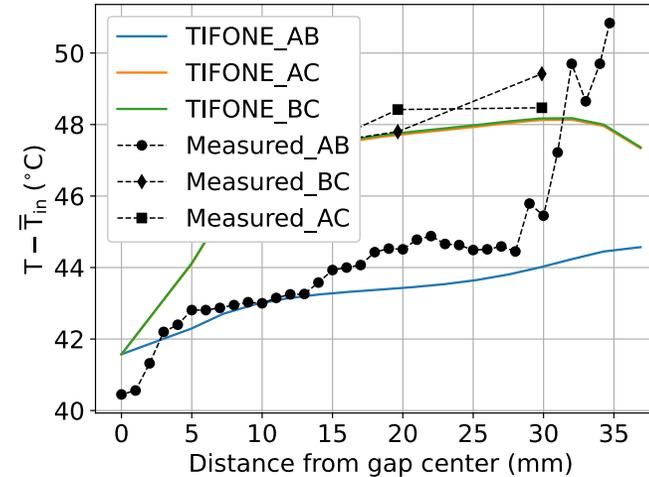
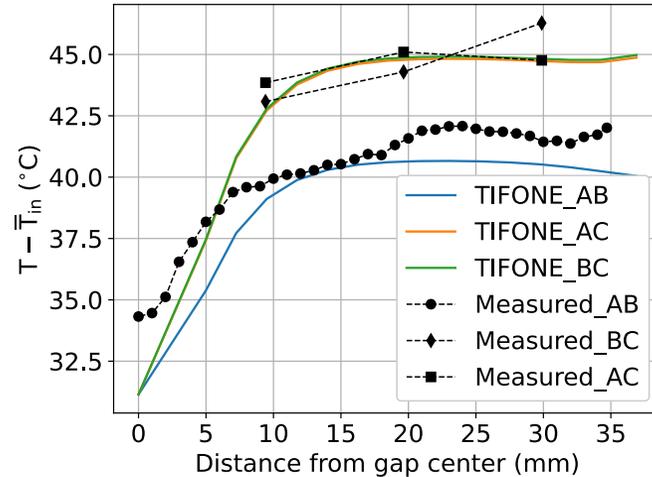
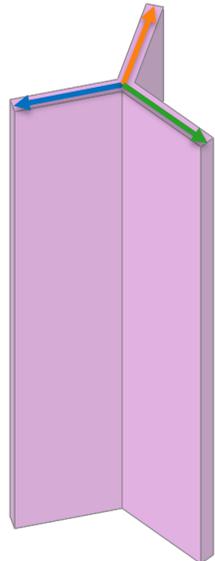
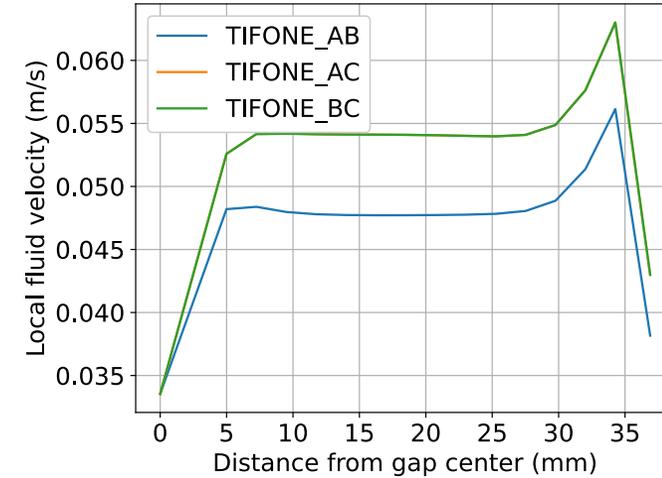
#3:  $Y_{mix} = 0.0038$



#6:  $Y_{mix} = 0.0056$



#8:  $Y_{mix} = 0.010$



- Conclusions:
  - A new DOC, TIFONE, was developed for the SC analysis of the IW flow and heat transfer in (H)LMCRs
  - Code development was performed according to ENEA Software Quality Assurance Procedures
  - Validation against KALLA experimental data shows promising results, which degrade towards the free convection
- Ongoing activities:
  - Benchmark against CFD (porous medium approach) for ATHENA core simulator
  - Inclusion in the ENEA DOC suite (e.g. to be coupled with ANTEO+)
- In perspective:
  - More validation data are needed to qualify the capabilities of the code in more reactor-relevant scenarios (e.g. ATHENA, CLEAR-S)
  - Empirical correlations for  $\varepsilon_{ij}$  and  $\kappa_{ij}$  might be derived from CFD calculations



**Politecnico  
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Department of Energy  
"G.Ferraris"

**nemo** | Nuclear Engineering  
MOdeling Group

*Thanks for your kind attention*



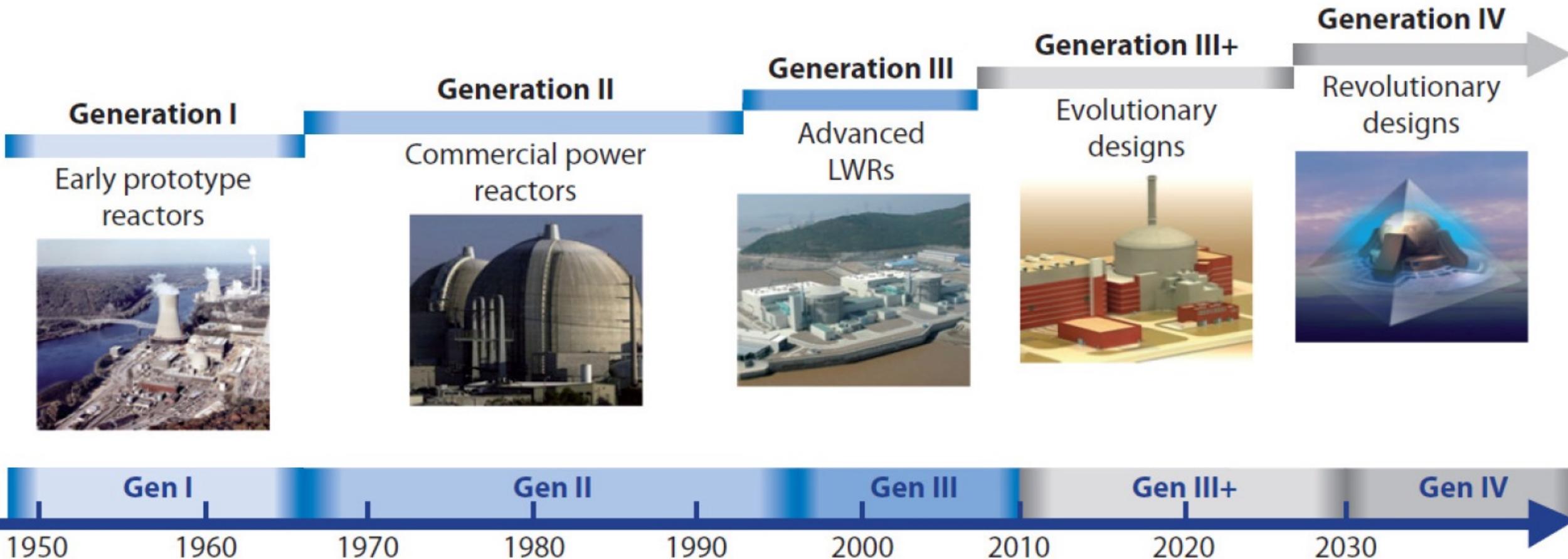
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Department of Energy  
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# Backup slides



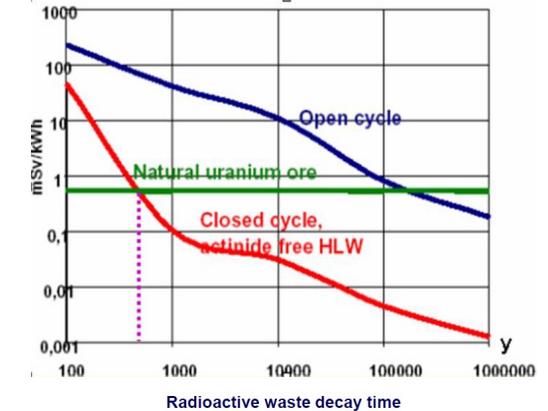
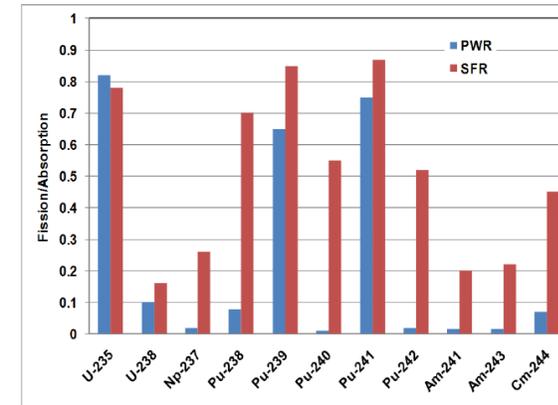
# Nuclear fission reactors generations



# Generation-IV fission reactors

- GIF objectives:
  - Sustainability
    - Improve **fuel utilization**
    - **Minimize long-term waste**
  - Economics
    - Reduce life cycle costs
    - Minimize financial risks
  - Safety and reliability:
    - Operational **safety** and reliability
    - Reduced core damage probability
    - Eliminate need for off-site power response
  - Proliferation resistance
- 6 potential reactor designs being considered

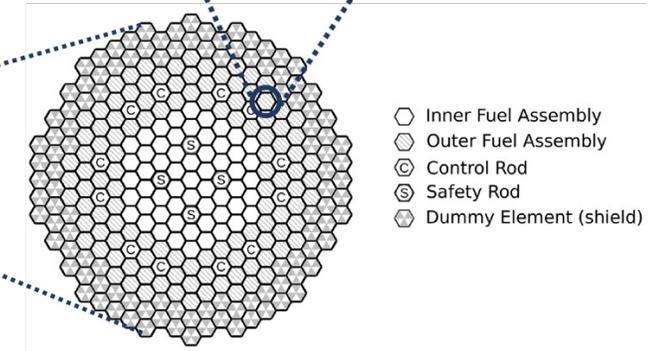
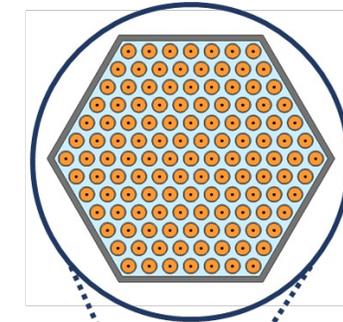
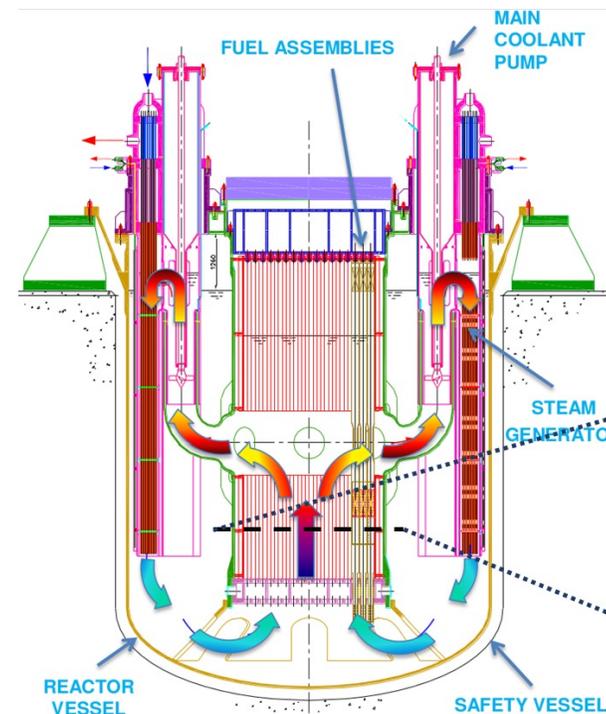
$$\frac{\int \sigma_f(E)\Phi(E)dE}{\int \Phi(E)dE} / \frac{\int \sigma_a(E)\Phi(E)dE}{\int \Phi(E)dE}$$



- Fast reactors:
  - Burn **MAAs** → **reduce long-term radiotoxicity**
  - Breed fuel → **fuel utilization efficiency**
  - Low moderation → need **large fissile inventory**
  - **Harsh neutron damage** (higher burnup, harder spectrum)

# HLMCRs: advantages and challenges

- Features of HLMCRs:
  - High core outlet temperature: **thermal efficiency** ↑
  - Large **margin to boiling**:
    - **No need for pressurization**
    - **No core voiding**
  - **Low reactivity** with air and water (vs. SFR)
  - **High heat transfer capability**
  - High coolant density
    - **natural circulation** for decay heat removal
    - Strong **coolant-structure interactions**
  - **Corrosion/erosion of structures**
  - Risk of **coolant freezing**
  - **Difficult inspection** (coolant opacity)



- Advanced Lead-cooled Fast Reactor European Demonstrator (ALFRED)

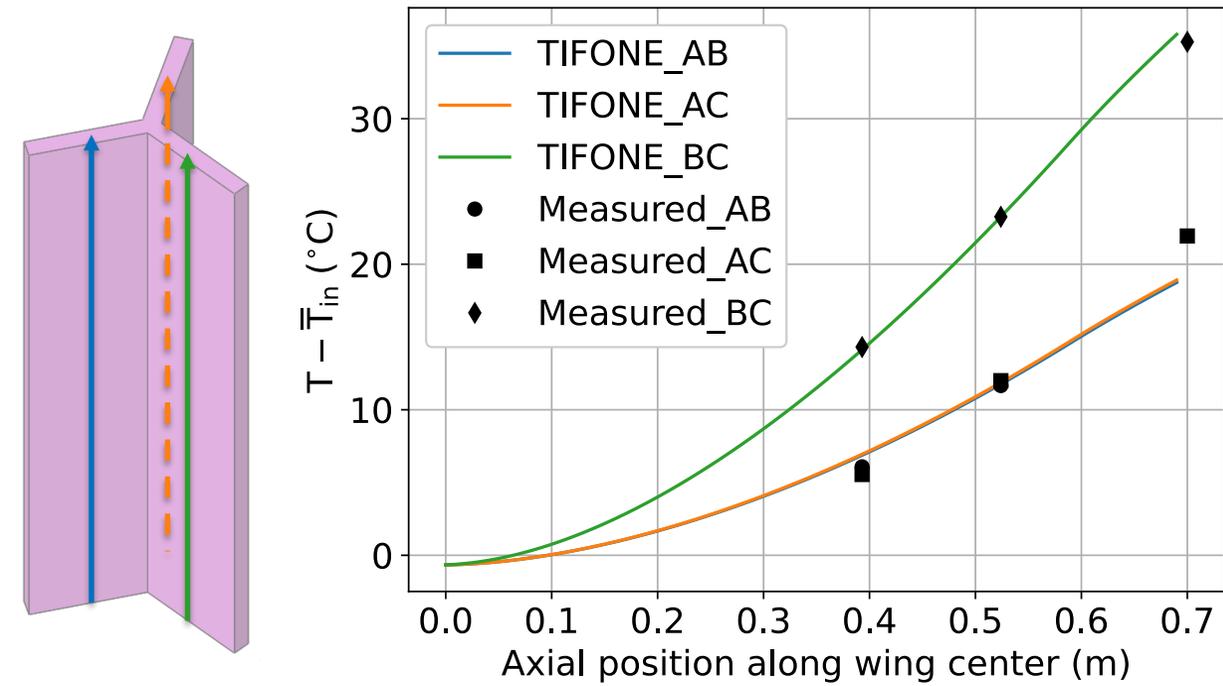
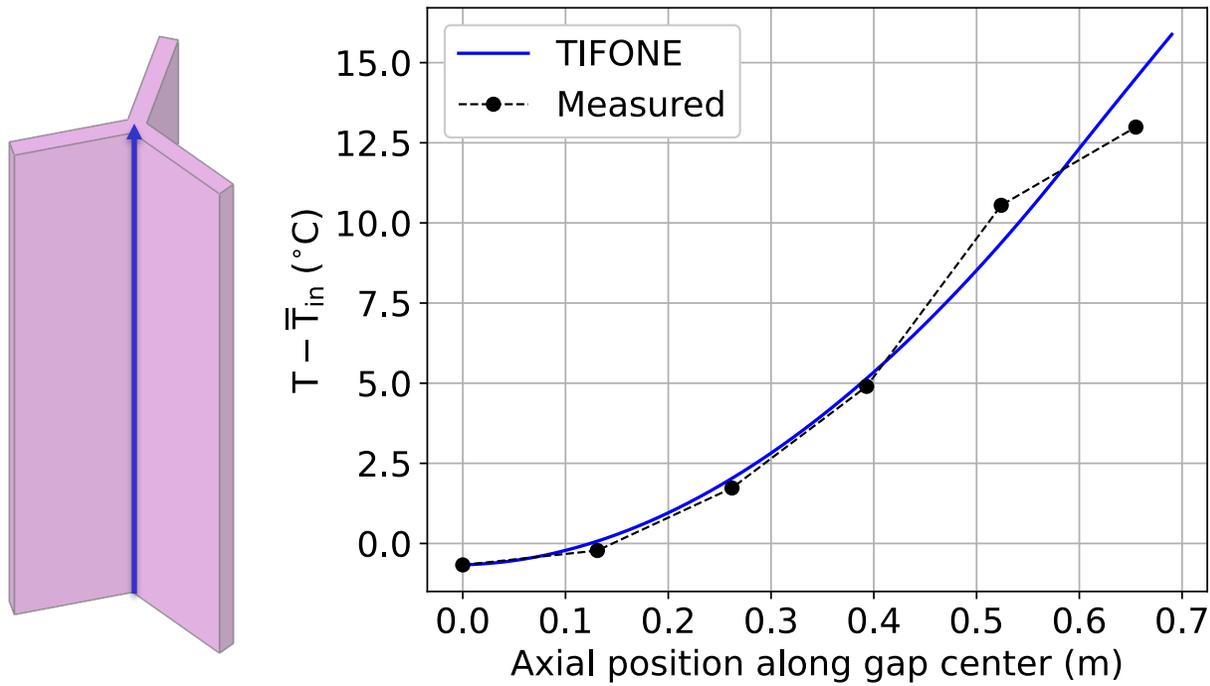
|                         |          |
|-------------------------|----------|
| Coolant inlet T         | 673 K    |
| Maximum fuel T          | ~2270 K  |
| Maximum core $\Delta p$ | 100 kPa  |
| Total electric power    | ~120 MWe |
| System efficiency       | ~40 %    |



# Asymmetric validation cases: unheated bundle A

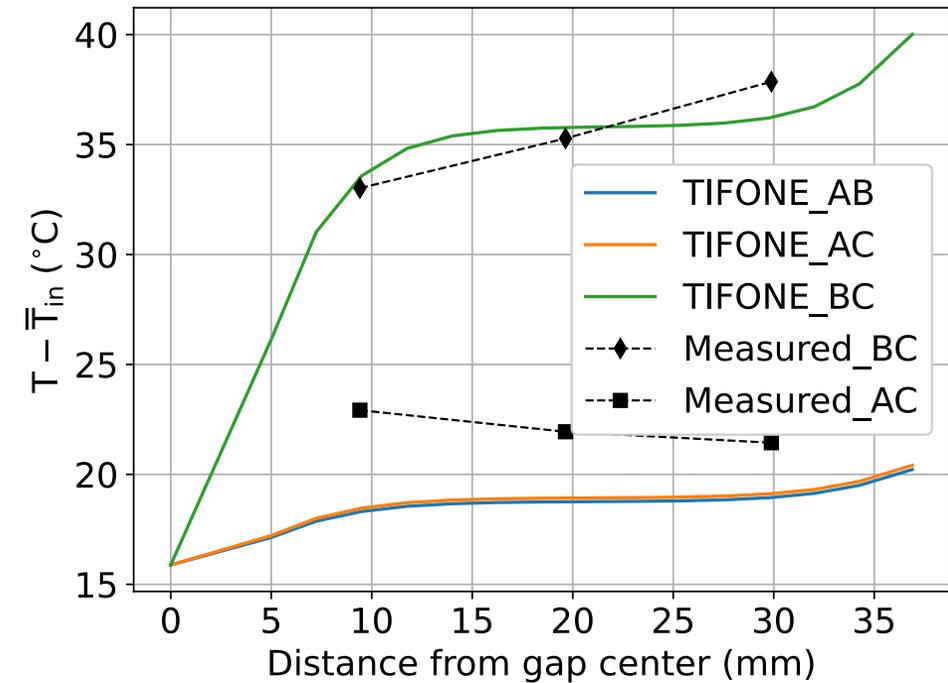
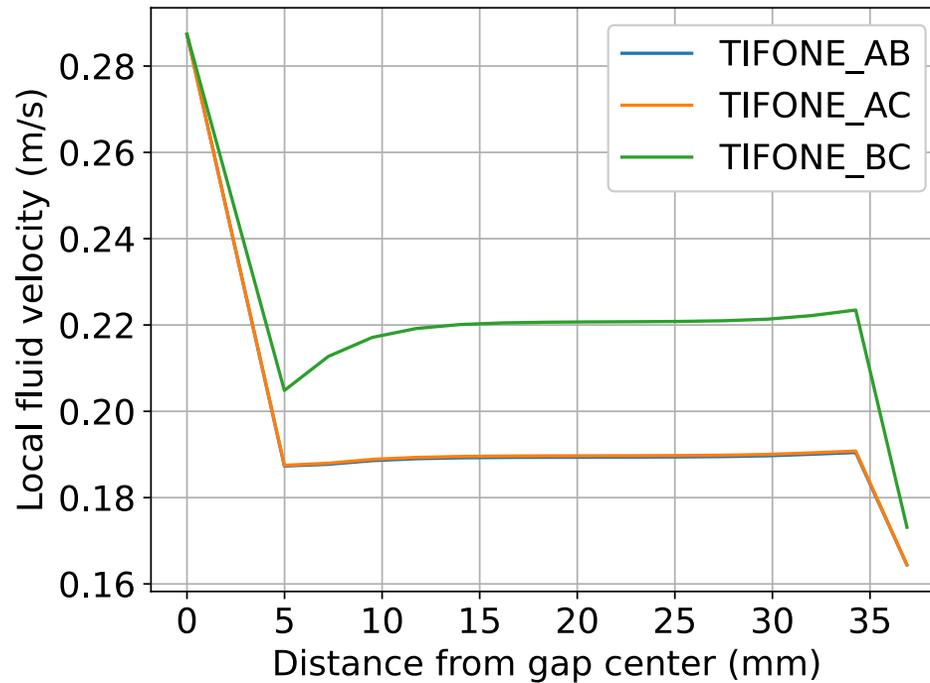
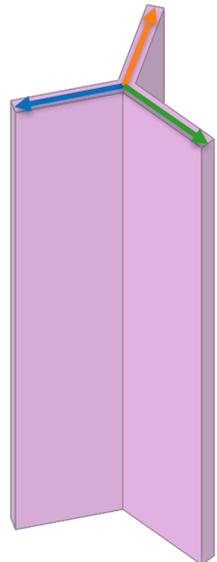
|     |                 |                 |                 |                 |                 |                 |                  |                  |                 |
|-----|-----------------|-----------------|-----------------|-----------------|-----------------|-----------------|------------------|------------------|-----------------|
| 011 | $199.2 \pm 0.2$ | $3.58 \pm 0.07$ | $3.58 \pm 0.07$ | $3.56 \pm 0.07$ | $0.69 \pm 0.01$ | $0.00 \pm 0.00$ | $30.00 \pm 0.30$ | $30.00 \pm 0.30$ | $232.1 \pm 0.2$ |
| 012 | $199.2 \pm 0.2$ | $3.58 \pm 0.07$ | $3.58 \pm 0.07$ | $3.56 \pm 0.07$ | $0.69 \pm 0.01$ | $0.00 \pm 0.00$ | $30.00 \pm 0.30$ | $30.00 \pm 0.30$ | $231.9 \pm 0.2$ |
| 013 | $199.2 \pm 0.2$ | $3.59 \pm 0.07$ | $3.60 \pm 0.07$ | $3.57 \pm 0.07$ | $0.52 \pm 0.01$ | $0.00 \pm 0.00$ | $30.00 \pm 0.30$ | $30.00 \pm 0.30$ | $232.6 \pm 0.2$ |
| 014 | $199.2 \pm 0.2$ | $3.59 \pm 0.07$ | $3.60 \pm 0.07$ | $3.57 \pm 0.07$ | $0.52 \pm 0.01$ | $0.00 \pm 0.00$ | $30.00 \pm 0.30$ | $30.00 \pm 0.30$ | $232.7 \pm 0.2$ |
| 015 | $199.1 \pm 0.2$ | $3.59 \pm 0.07$ | $3.59 \pm 0.07$ | $3.57 \pm 0.07$ | $0.34 \pm 0.01$ | $0.00 \pm 0.00$ | $30.00 \pm 0.30$ | $30.00 \pm 0.30$ | $233.4 \pm 0.2$ |
| 016 | $199.1 \pm 0.2$ | $3.59 \pm 0.07$ | $3.59 \pm 0.07$ | $3.57 \pm 0.07$ | $0.34 \pm 0.01$ | $0.00 \pm 0.00$ | $30.00 \pm 0.30$ | $30.00 \pm 0.30$ | $233.4 \pm 0.2$ |
| 017 | $199.1 \pm 0.2$ | $3.60 \pm 0.07$ | $3.60 \pm 0.07$ | $3.57 \pm 0.07$ | $0.17 \pm 0.00$ | $0.00 \pm 0.00$ | $30.00 \pm 0.30$ | $30.00 \pm 0.30$ | $233.8 \pm 0.2$ |
| 018 | $199.1 \pm 0.2$ | $3.60 \pm 0.07$ | $3.60 \pm 0.07$ | $3.57 \pm 0.07$ | $0.17 \pm 0.00$ | $0.00 \pm 0.00$ | $30.00 \pm 0.30$ | $30.00 \pm 0.30$ | $233.6 \pm 0.2$ |

# Asymmetric case #11: axial temperature profiles



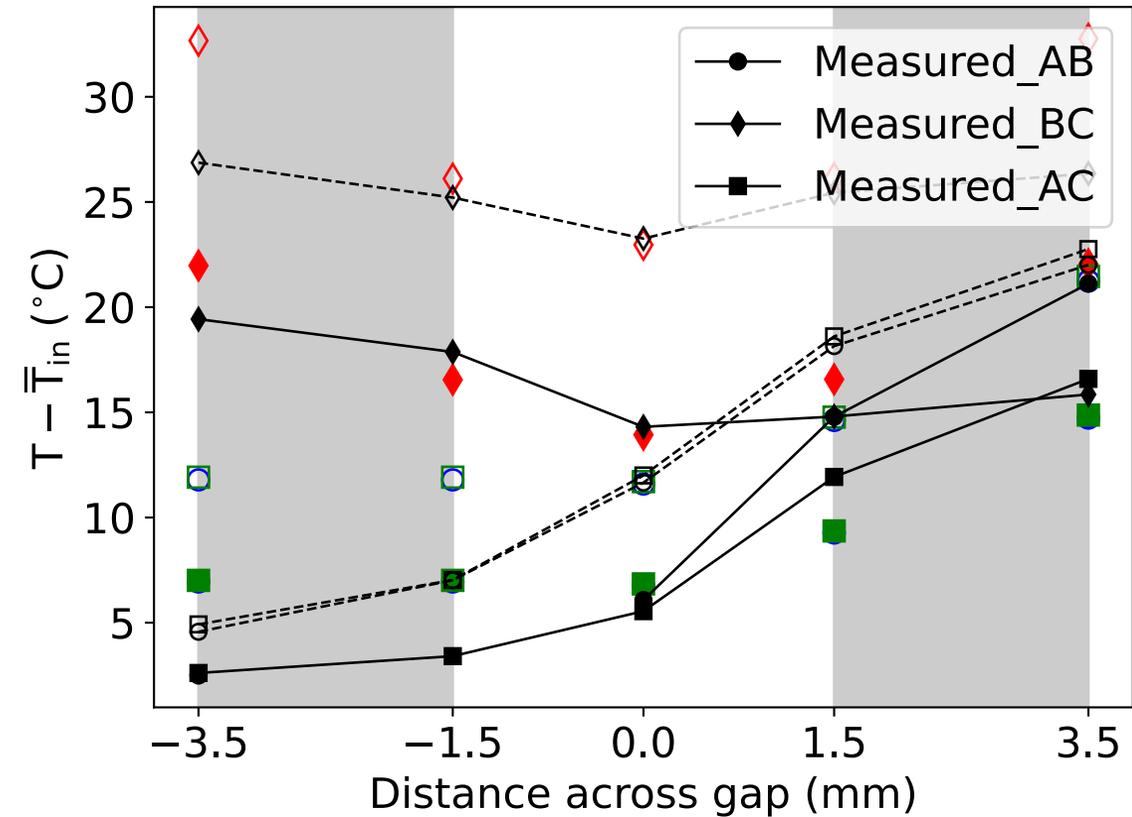
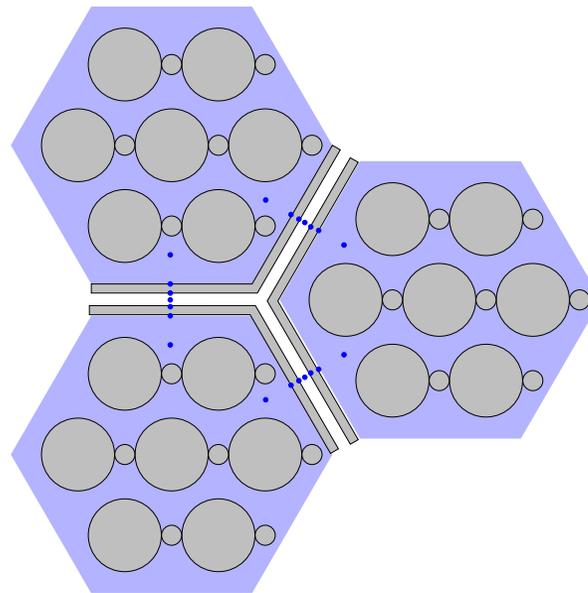


# Asymmetric case #11: radial temperature profiles

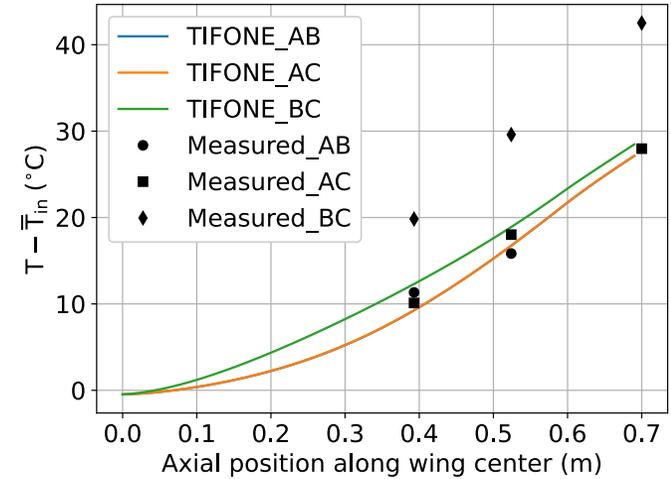
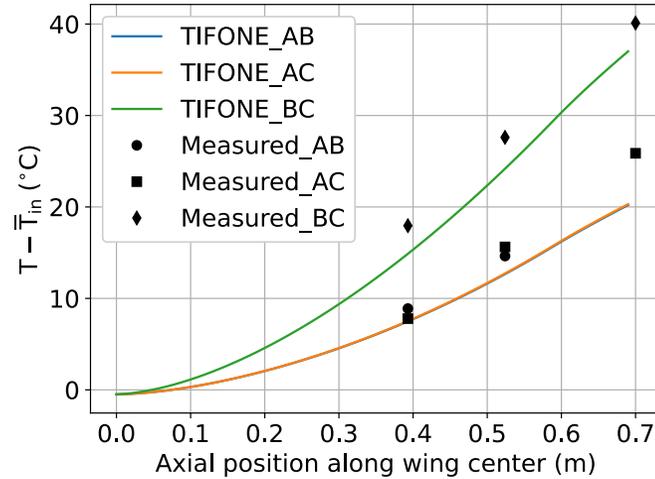
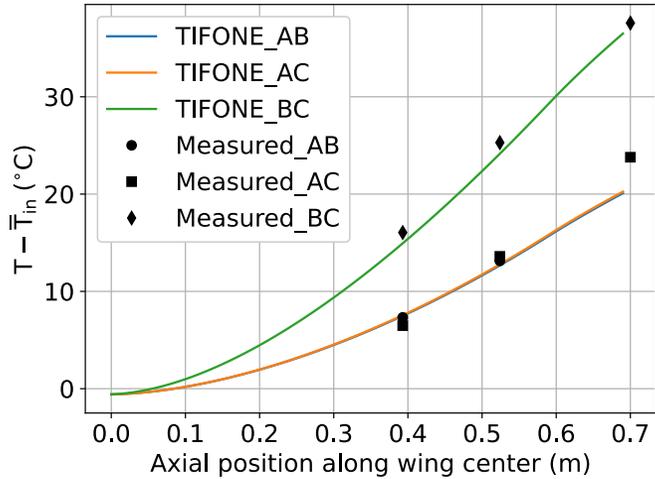
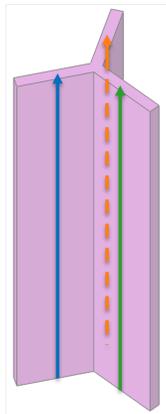
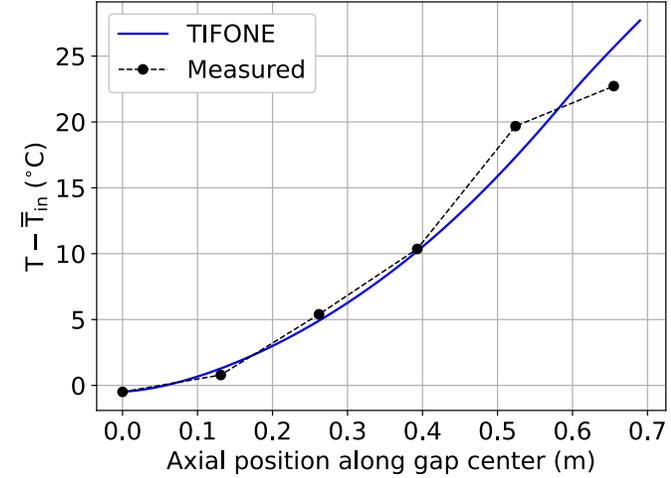
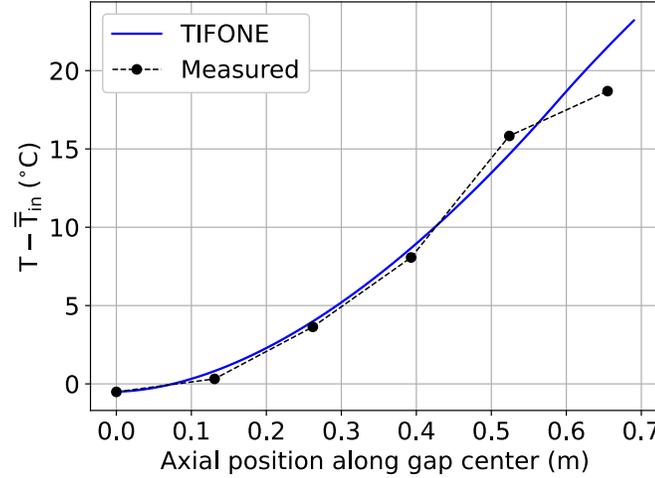
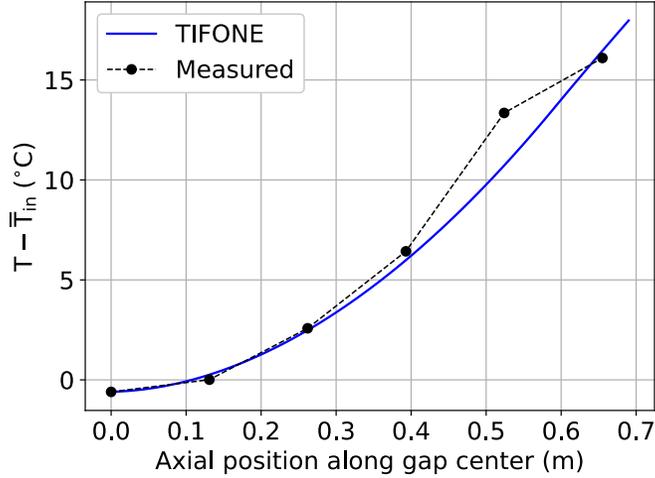
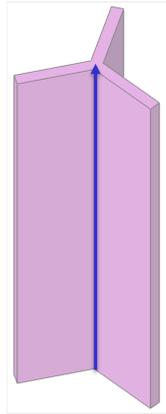




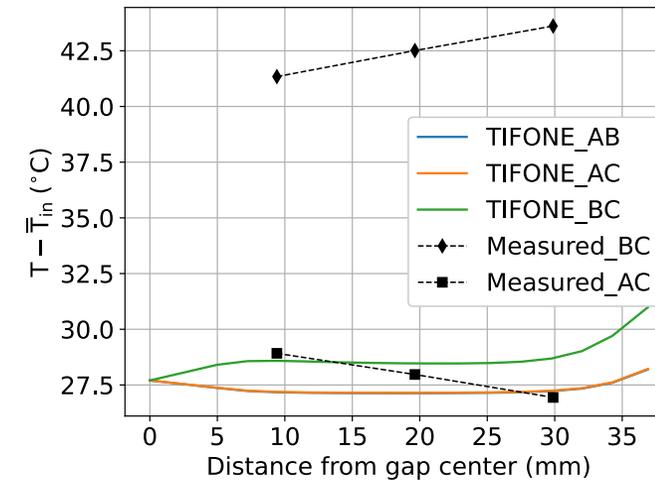
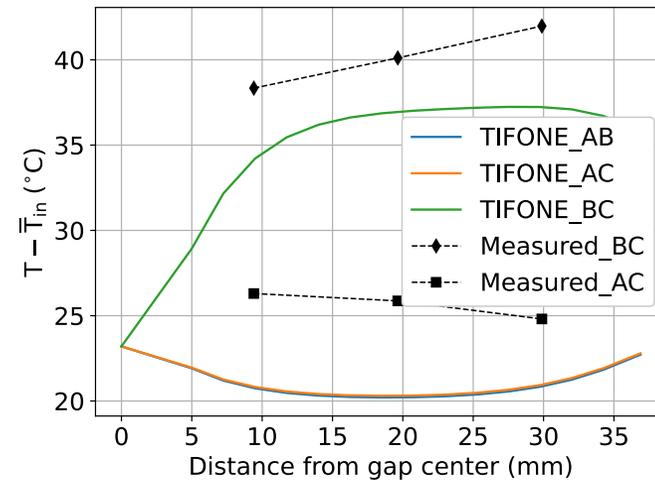
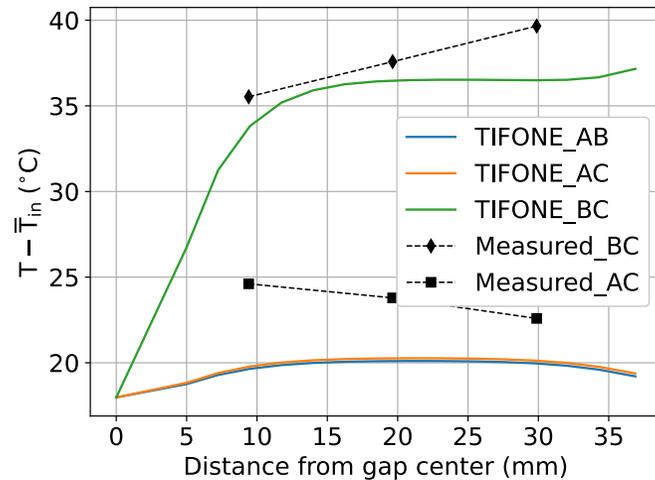
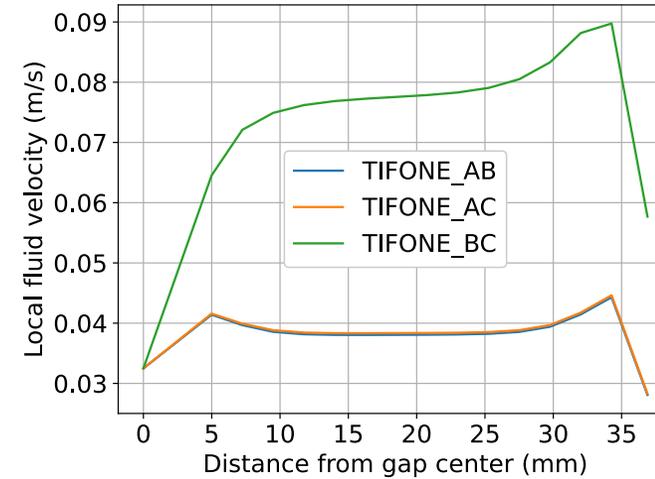
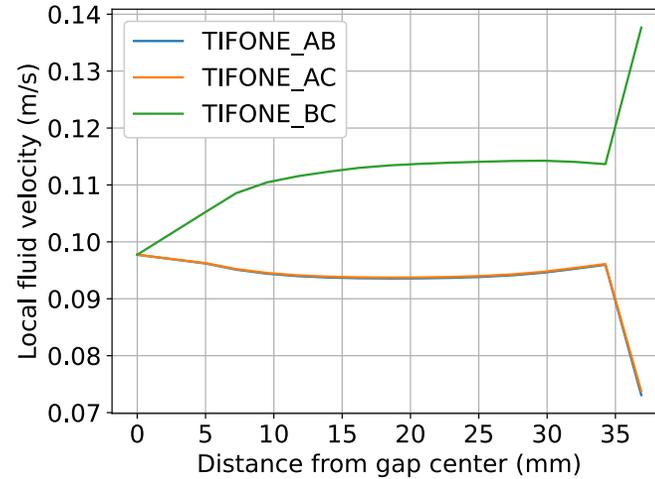
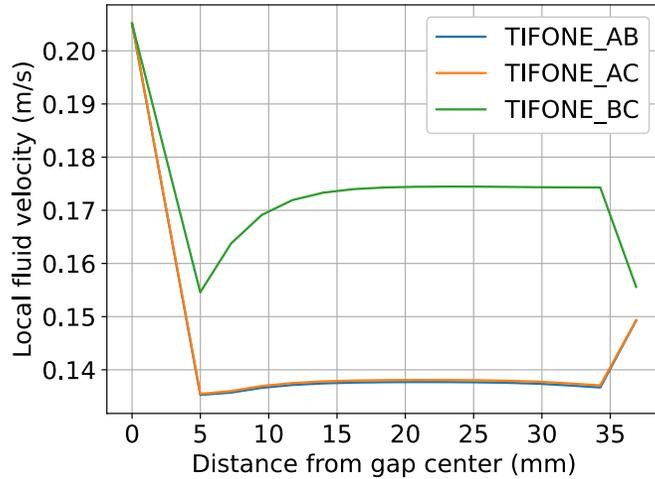
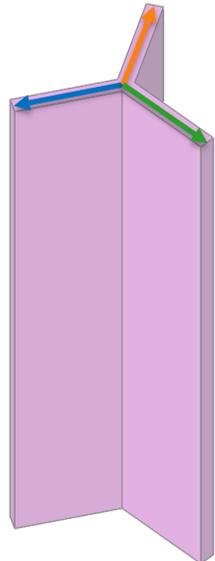
# Asymmetric case #11: wrapper temperatures



# Asymmetric cases # 13,15,17: axial temperature profiles



# Asymmetric cases # 13,15,17: radial velocity and temperature profiles





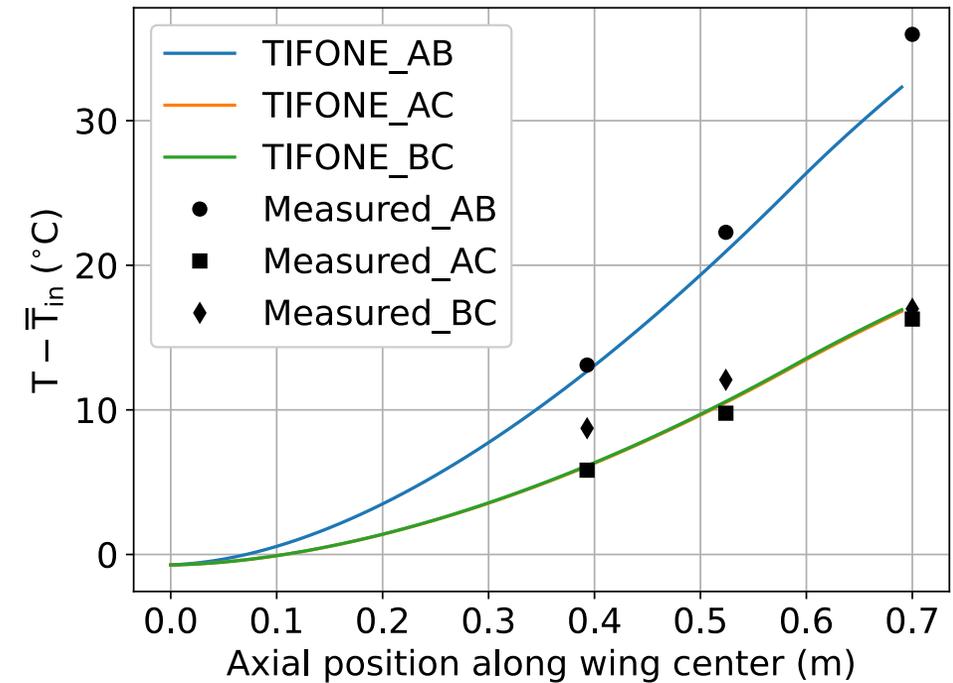
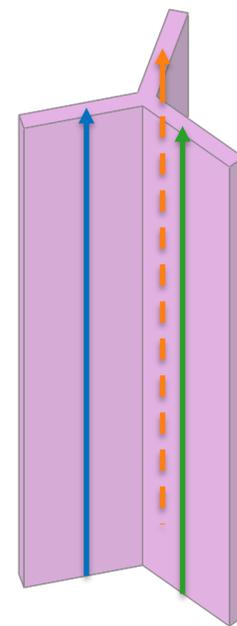
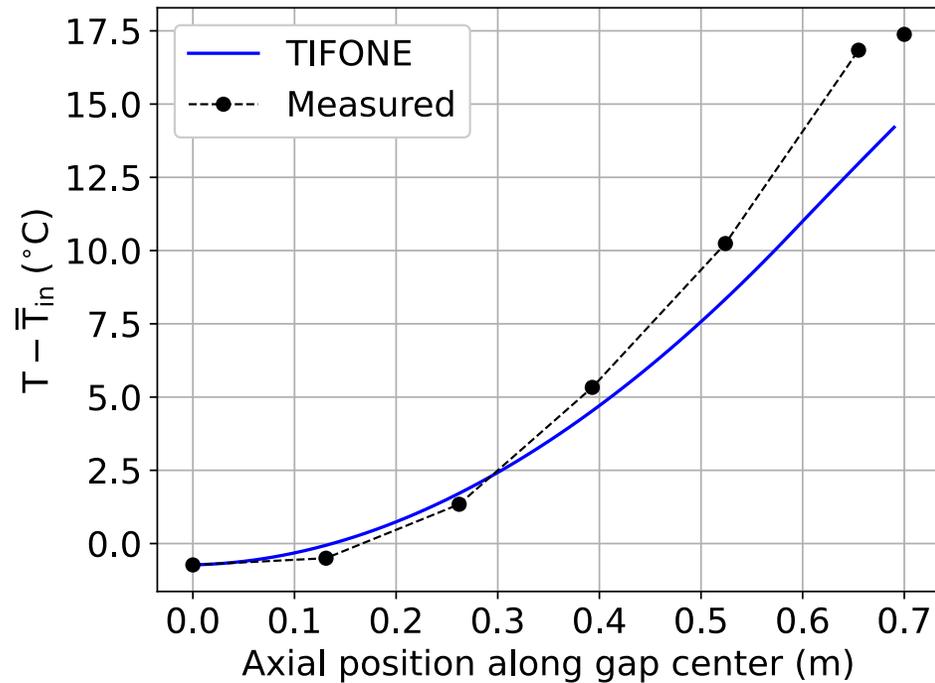
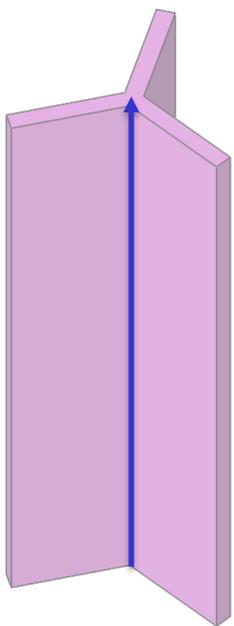
# Aymmetric validation cases: unheated bundle C

|     |                 |                 |                 |                 |                 |                  |                  |                 |                 |
|-----|-----------------|-----------------|-----------------|-----------------|-----------------|------------------|------------------|-----------------|-----------------|
| 031 | $199.2 \pm 0.2$ | $3.59 \pm 0.07$ | $3.58 \pm 0.07$ | $3.55 \pm 0.07$ | $0.69 \pm 0.01$ | $30.00 \pm 0.30$ | $30.00 \pm 0.30$ | $0.00 \pm 0.00$ | $231.8 \pm 0.2$ |
| 032 | $199.2 \pm 0.2$ | $3.60 \pm 0.07$ | $3.58 \pm 0.07$ | $3.55 \pm 0.07$ | $0.69 \pm 0.01$ | $30.00 \pm 0.30$ | $30.00 \pm 0.30$ | $0.00 \pm 0.00$ | $231.8 \pm 0.2$ |
| 033 | $199.1 \pm 0.2$ | $3.59 \pm 0.07$ | $3.59 \pm 0.07$ | $3.57 \pm 0.07$ | $0.52 \pm 0.01$ | $30.00 \pm 0.30$ | $30.00 \pm 0.30$ | $0.00 \pm 0.00$ | $232.1 \pm 0.2$ |
| 034 | $199.1 \pm 0.2$ | $3.59 \pm 0.07$ | $3.59 \pm 0.07$ | $3.57 \pm 0.07$ | $0.52 \pm 0.01$ | $30.00 \pm 0.30$ | $30.00 \pm 0.30$ | $0.00 \pm 0.00$ | $232.2 \pm 0.2$ |
| 035 | $199.1 \pm 0.2$ | $3.60 \pm 0.07$ | $3.59 \pm 0.07$ | $3.60 \pm 0.07$ | $0.34 \pm 0.01$ | $30.00 \pm 0.30$ | $30.00 \pm 0.30$ | $0.00 \pm 0.00$ | $232.2 \pm 0.2$ |
| 036 | $199.1 \pm 0.2$ | $3.60 \pm 0.07$ | $3.59 \pm 0.07$ | $3.60 \pm 0.07$ | $0.34 \pm 0.01$ | $30.00 \pm 0.30$ | $30.00 \pm 0.30$ | $0.00 \pm 0.00$ | $232.4 \pm 0.2$ |
| 037 | $199.1 \pm 0.2$ | $3.57 \pm 0.07$ | $3.57 \pm 0.07$ | $3.58 \pm 0.07$ | $0.17 \pm 0.00$ | $30.00 \pm 0.30$ | $30.00 \pm 0.30$ | $0.00 \pm 0.00$ | $233.1 \pm 0.2$ |
| 038 | $199.0 \pm 0.2$ | $3.57 \pm 0.07$ | $3.57 \pm 0.07$ | $3.58 \pm 0.07$ | $0.17 \pm 0.00$ | $30.00 \pm 0.30$ | $30.00 \pm 0.30$ | $0.00 \pm 0.00$ | $232.9 \pm 0.2$ |

*Note: in this case calorimetric measurements were unavailable  $\rightarrow$  use  $q_{tot}$  as computed by ANTEO+*

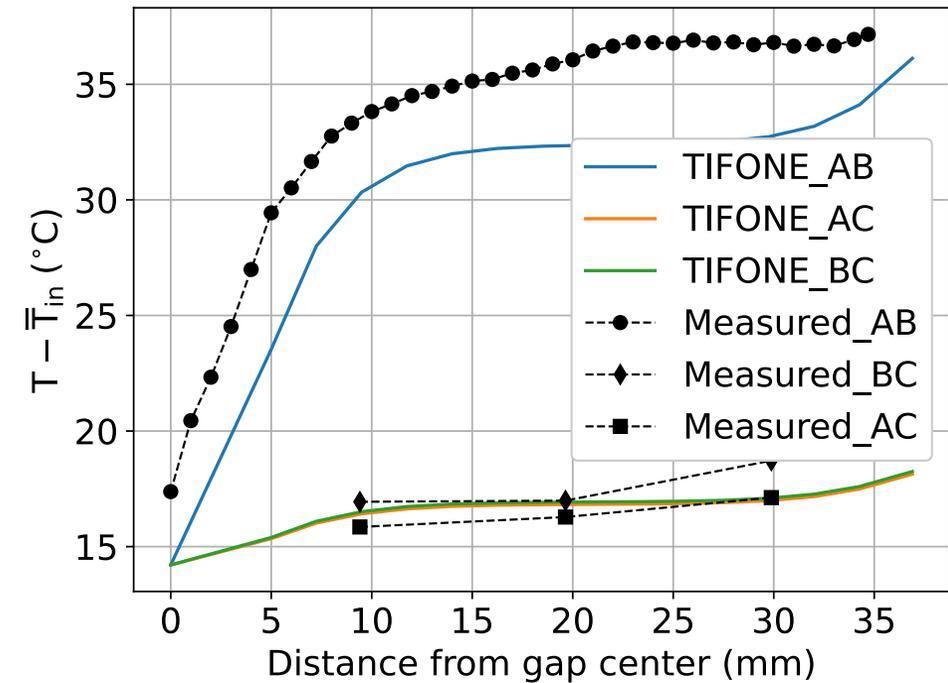
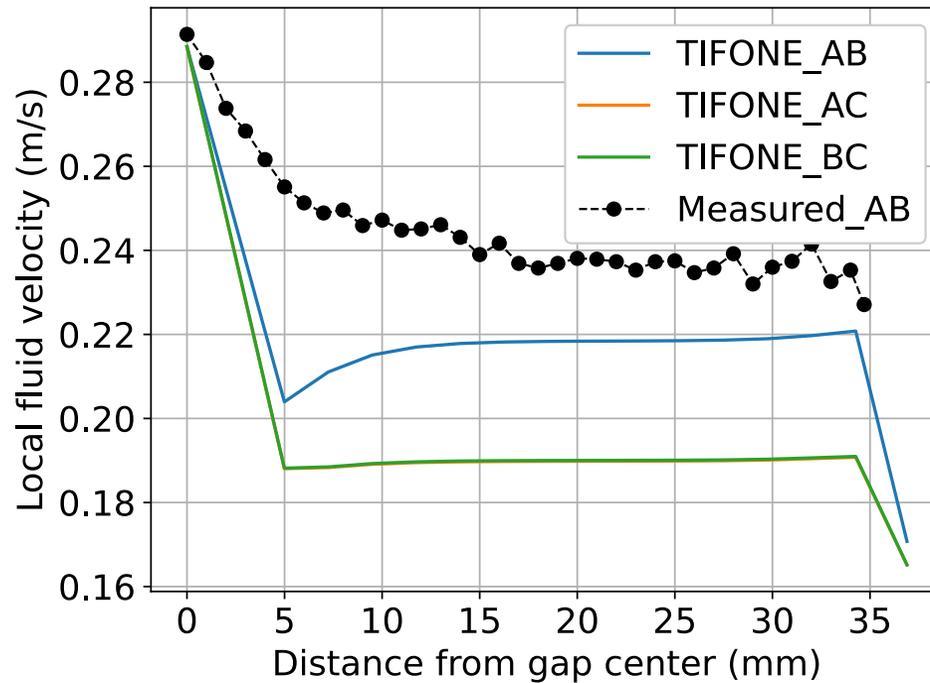
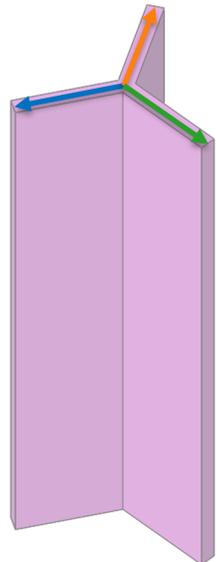


# Asymmetric case #32: axial temperature profiles



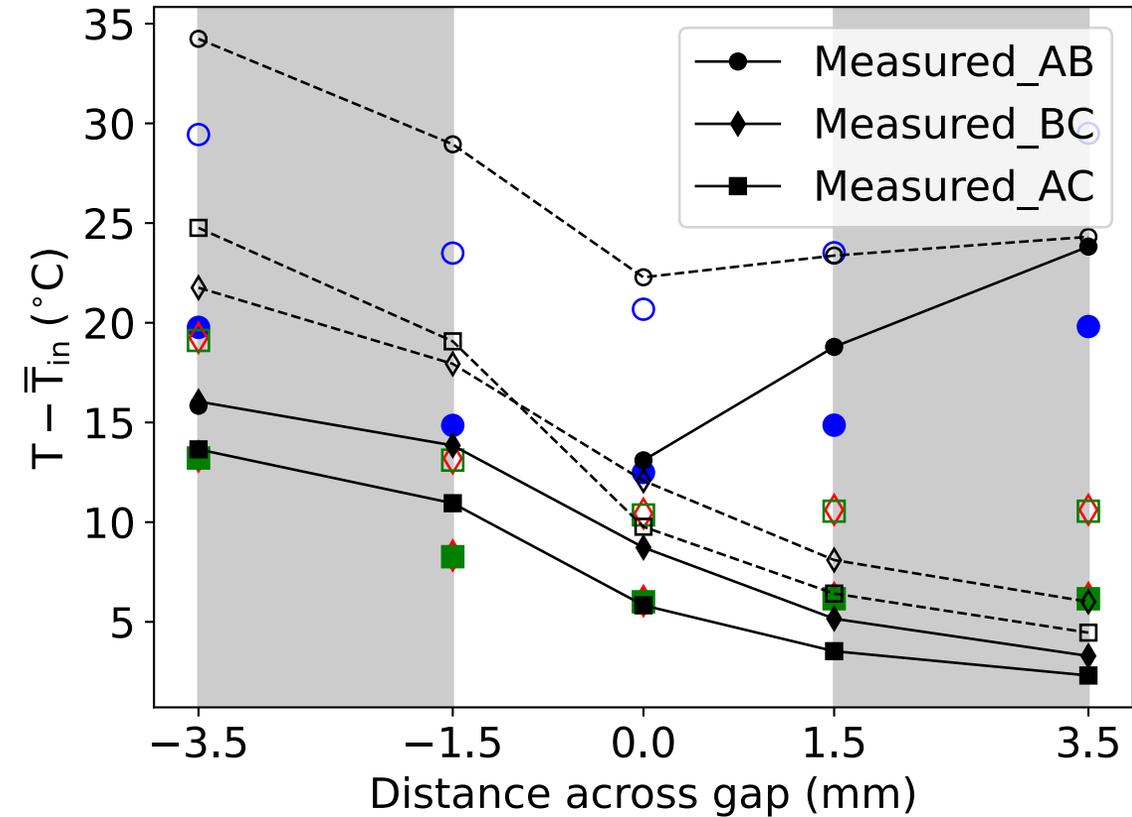
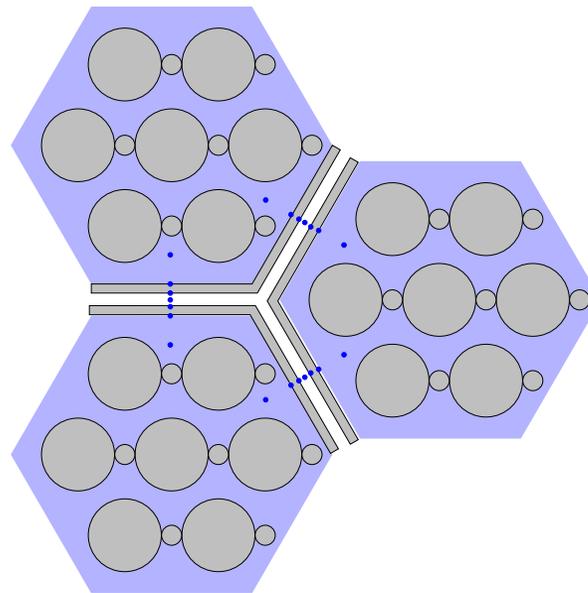


# Asymmetric case #32: radial temperature profiles

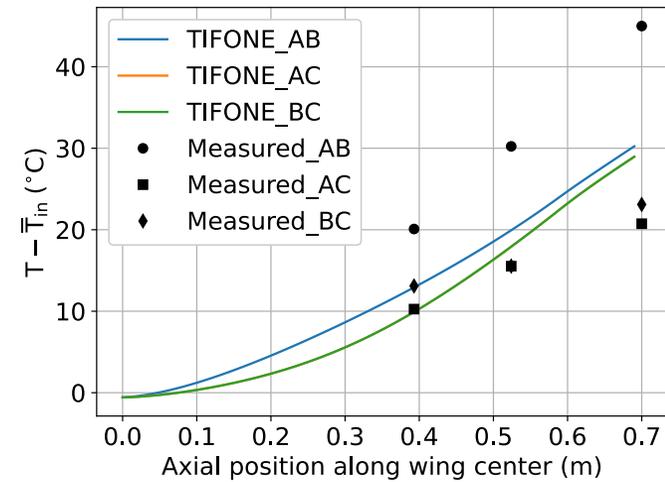
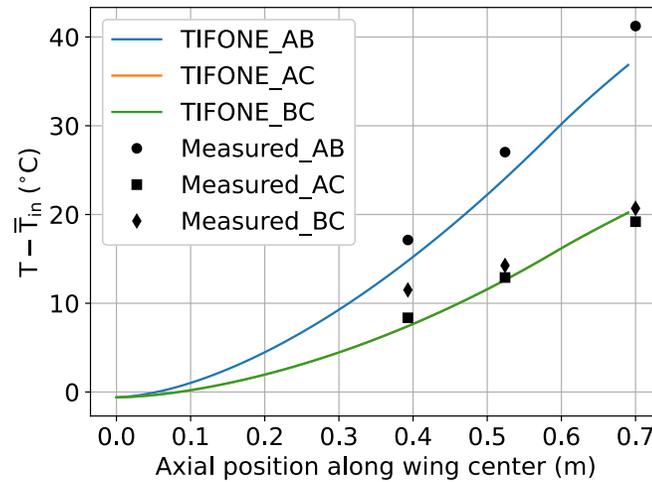
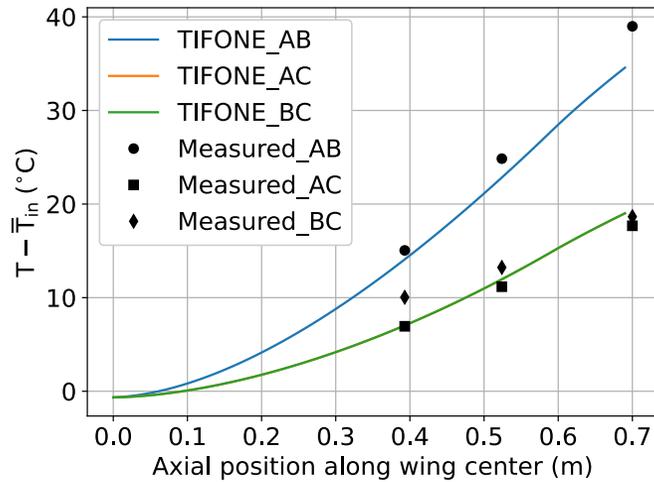
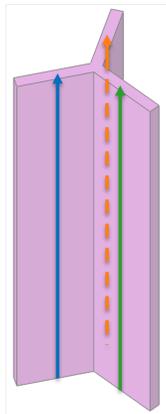
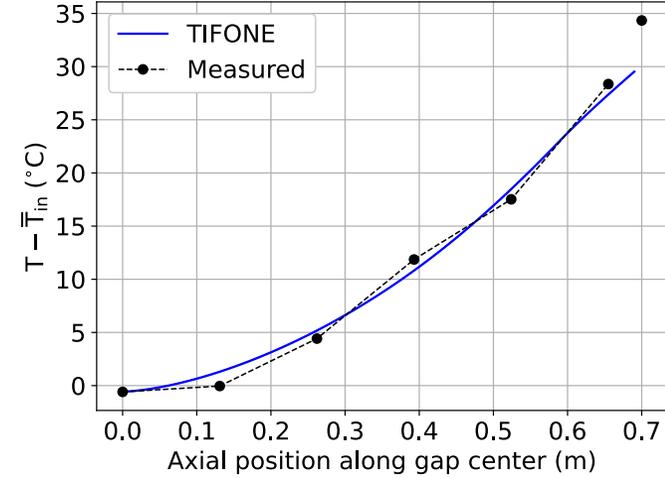
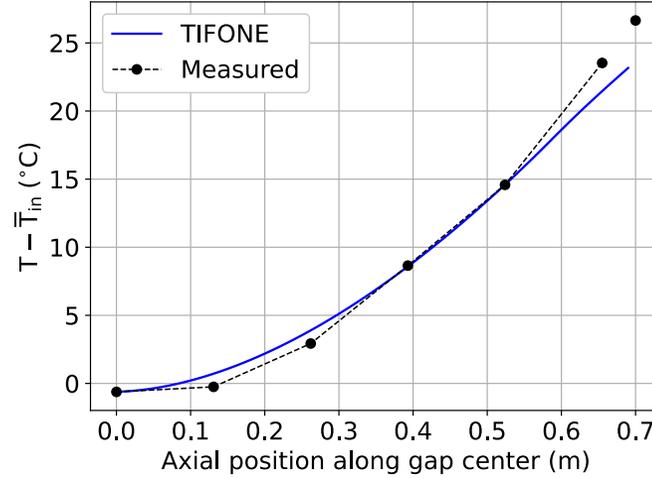
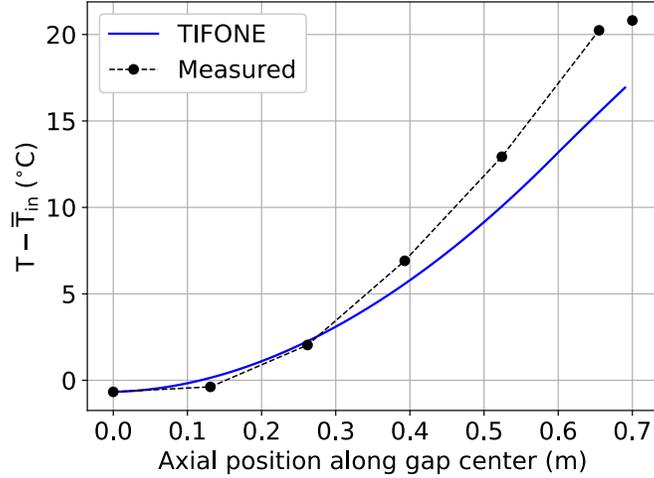
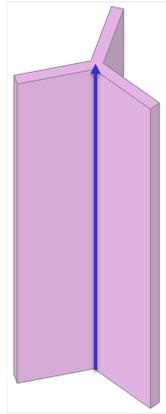




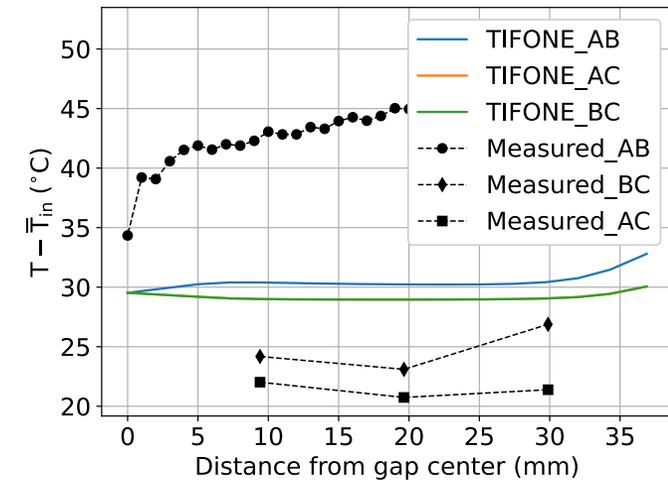
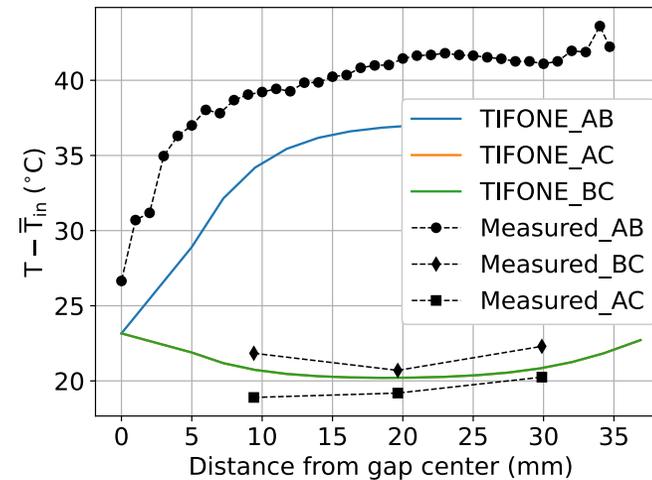
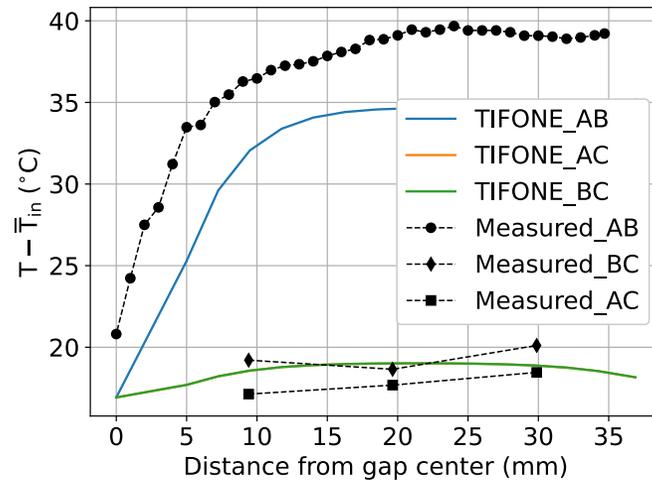
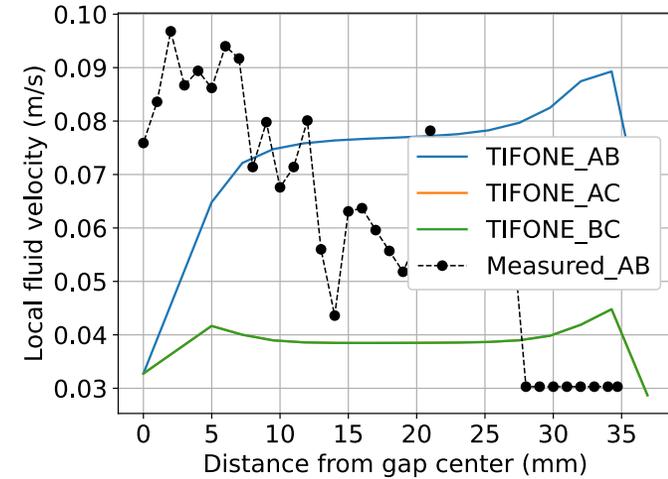
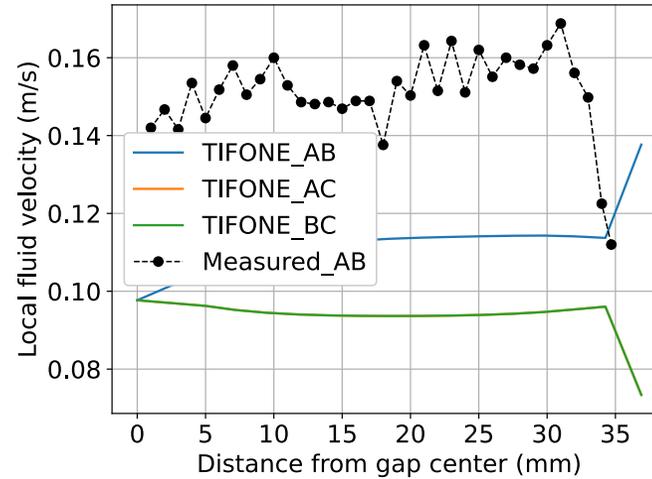
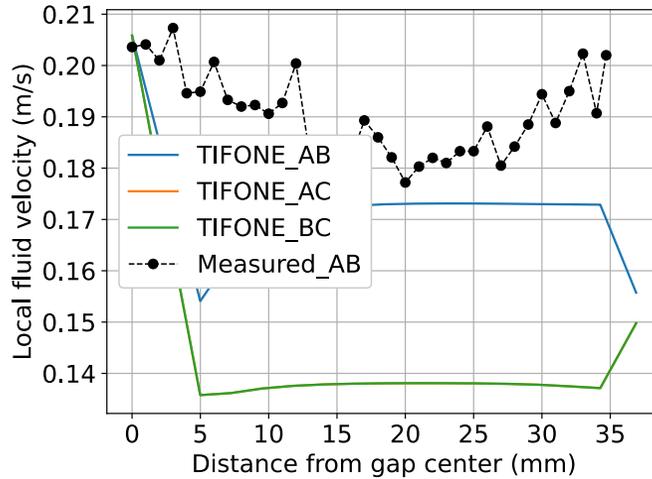
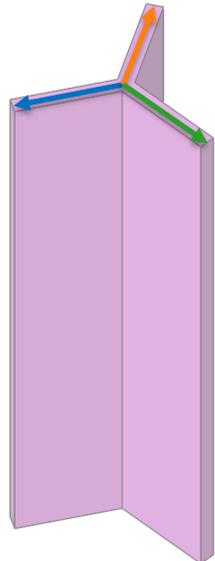
# Asymmetric case #32: wrapper temperatures



# Asymmetric cases # 34,36,38: axial temperature profiles



# Asymmetric cases # 34,36,38: radial temperature profiles

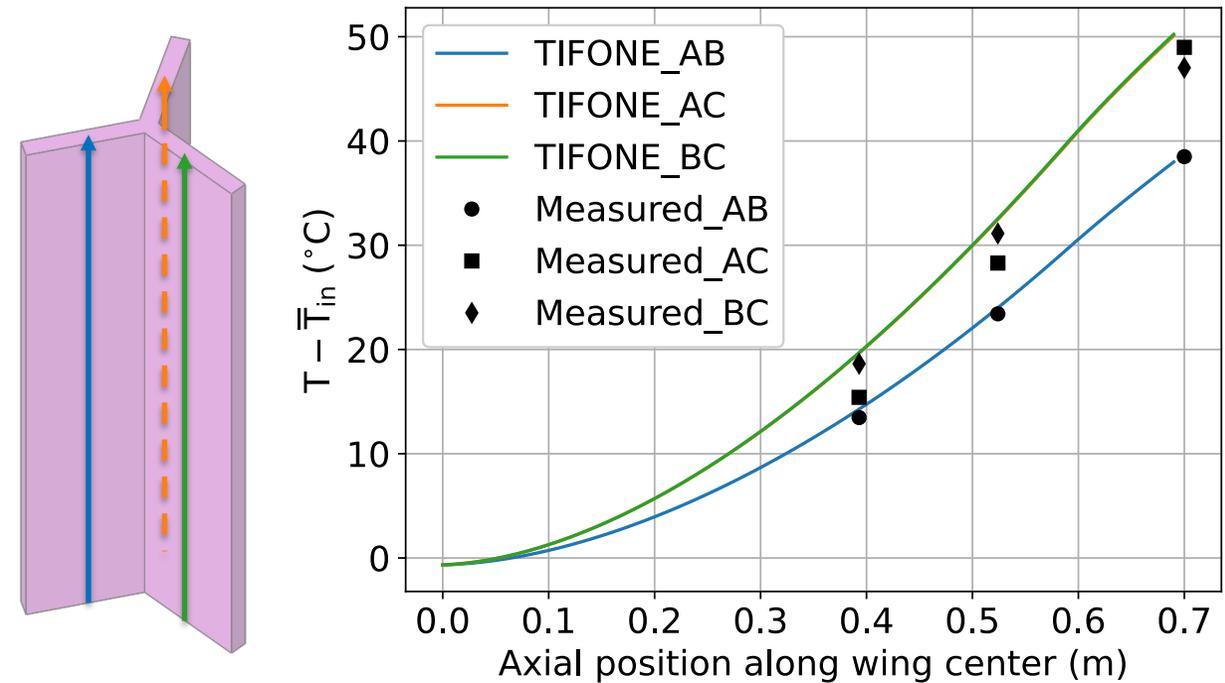
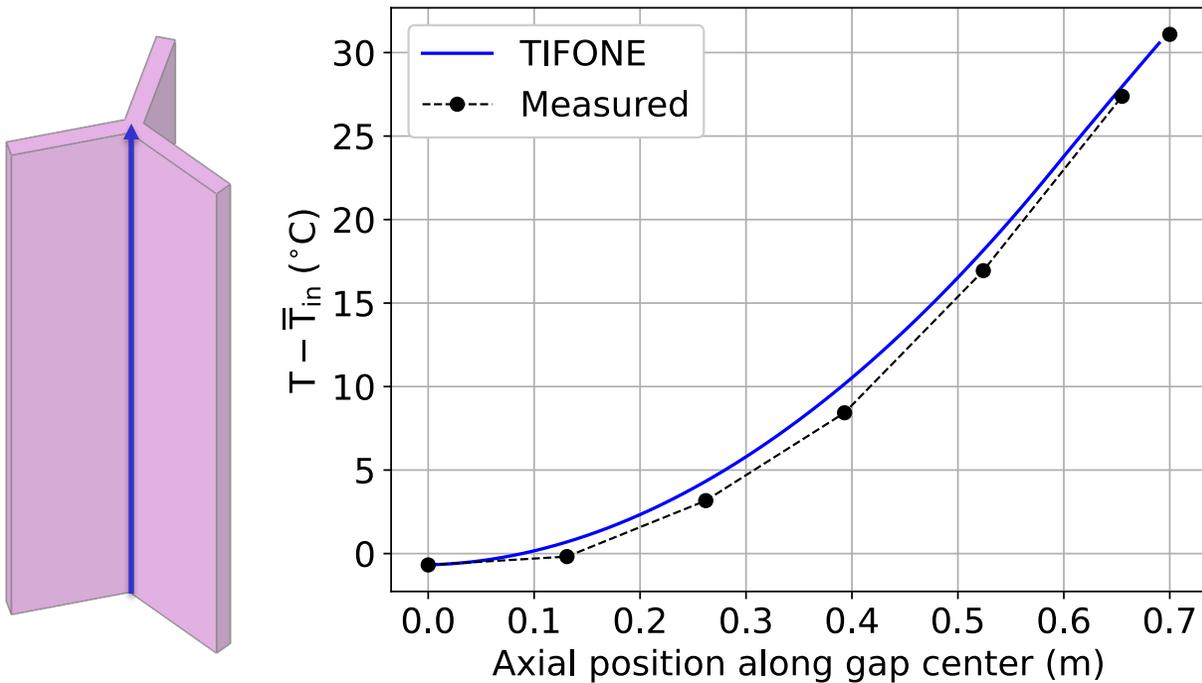




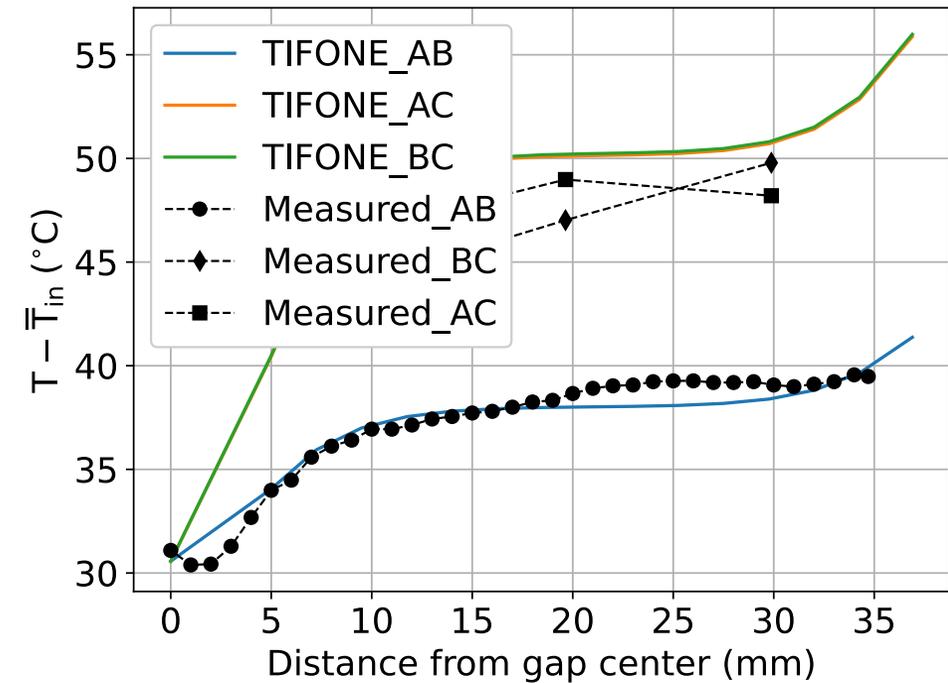
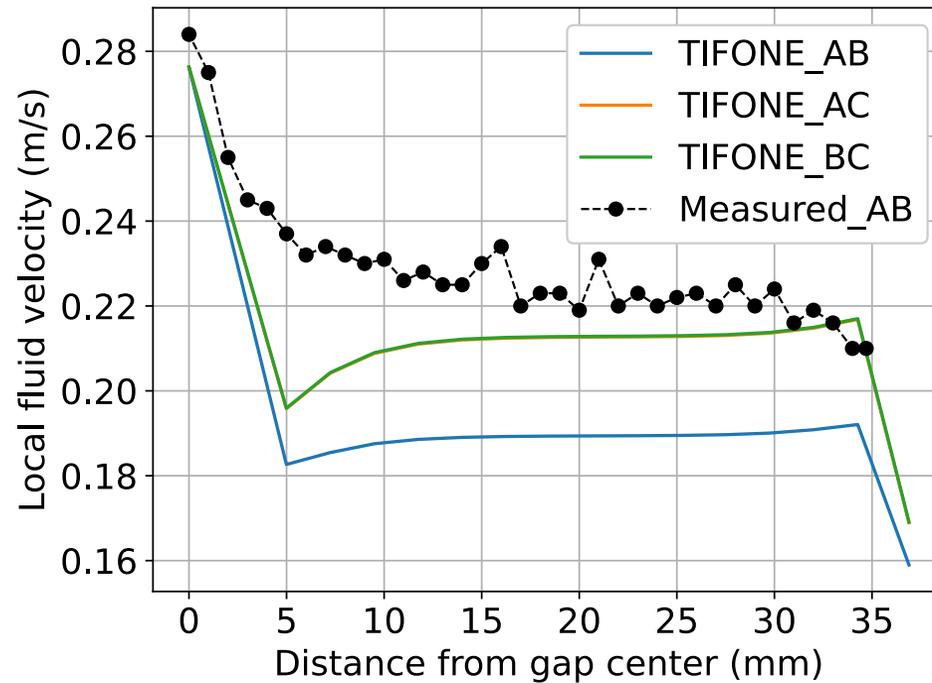
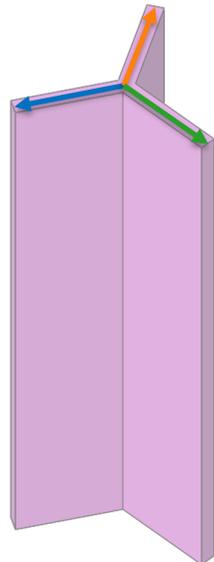
# Aymmetric validation cases: reduced flow rate in C by 40%

|     |                 |                 |                 |                 |                 |                  |                  |                  |                 |
|-----|-----------------|-----------------|-----------------|-----------------|-----------------|------------------|------------------|------------------|-----------------|
| 054 | $199.1 \pm 0.2$ | $3.60 \pm 0.07$ | $3.58 \pm 0.07$ | $2.22 \pm 0.04$ | $0.69 \pm 0.01$ | $30.00 \pm 0.30$ | $30.00 \pm 0.30$ | $30.00 \pm 0.30$ | $255.0 \pm 0.2$ |
| 055 | $199.1 \pm 0.2$ | $3.60 \pm 0.07$ | $3.58 \pm 0.07$ | $2.21 \pm 0.04$ | $0.69 \pm 0.01$ | $30.00 \pm 0.30$ | $30.00 \pm 0.30$ | $30.00 \pm 0.30$ | $255.0 \pm 0.2$ |
| 056 | $199.1 \pm 0.2$ | $3.59 \pm 0.07$ | $3.58 \pm 0.07$ | $2.15 \pm 0.04$ | $0.51 \pm 0.01$ | $30.00 \pm 0.30$ | $30.00 \pm 0.30$ | $30.00 \pm 0.30$ | $256.9 \pm 0.2$ |
| 057 | $199.1 \pm 0.2$ | $3.58 \pm 0.07$ | $3.58 \pm 0.07$ | $2.15 \pm 0.04$ | $0.51 \pm 0.01$ | $30.00 \pm 0.30$ | $30.00 \pm 0.30$ | $30.00 \pm 0.30$ | $256.9 \pm 0.2$ |
| 058 | $199.1 \pm 0.2$ | $3.59 \pm 0.07$ | $3.58 \pm 0.07$ | $2.15 \pm 0.04$ | $0.34 \pm 0.01$ | $30.00 \pm 0.30$ | $30.00 \pm 0.30$ | $30.00 \pm 0.30$ | $257.8 \pm 0.2$ |
| 059 | $199.0 \pm 0.2$ | $3.58 \pm 0.07$ | $3.58 \pm 0.07$ | $2.15 \pm 0.04$ | $0.34 \pm 0.01$ | $30.00 \pm 0.30$ | $30.00 \pm 0.30$ | $30.00 \pm 0.30$ | $257.8 \pm 0.2$ |
| 060 | $199.0 \pm 0.2$ | $3.58 \pm 0.07$ | $3.57 \pm 0.07$ | $2.15 \pm 0.04$ | $0.17 \pm 0.00$ | $30.00 \pm 0.30$ | $30.00 \pm 0.30$ | $30.00 \pm 0.30$ | $259.0 \pm 0.2$ |
| 061 | $199.0 \pm 0.2$ | $3.58 \pm 0.07$ | $3.57 \pm 0.07$ | $2.15 \pm 0.04$ | $0.17 \pm 0.00$ | $30.00 \pm 0.30$ | $30.00 \pm 0.30$ | $30.00 \pm 0.30$ | $259.0 \pm 0.2$ |

# Aymmetric case #55: axial temperature profiles

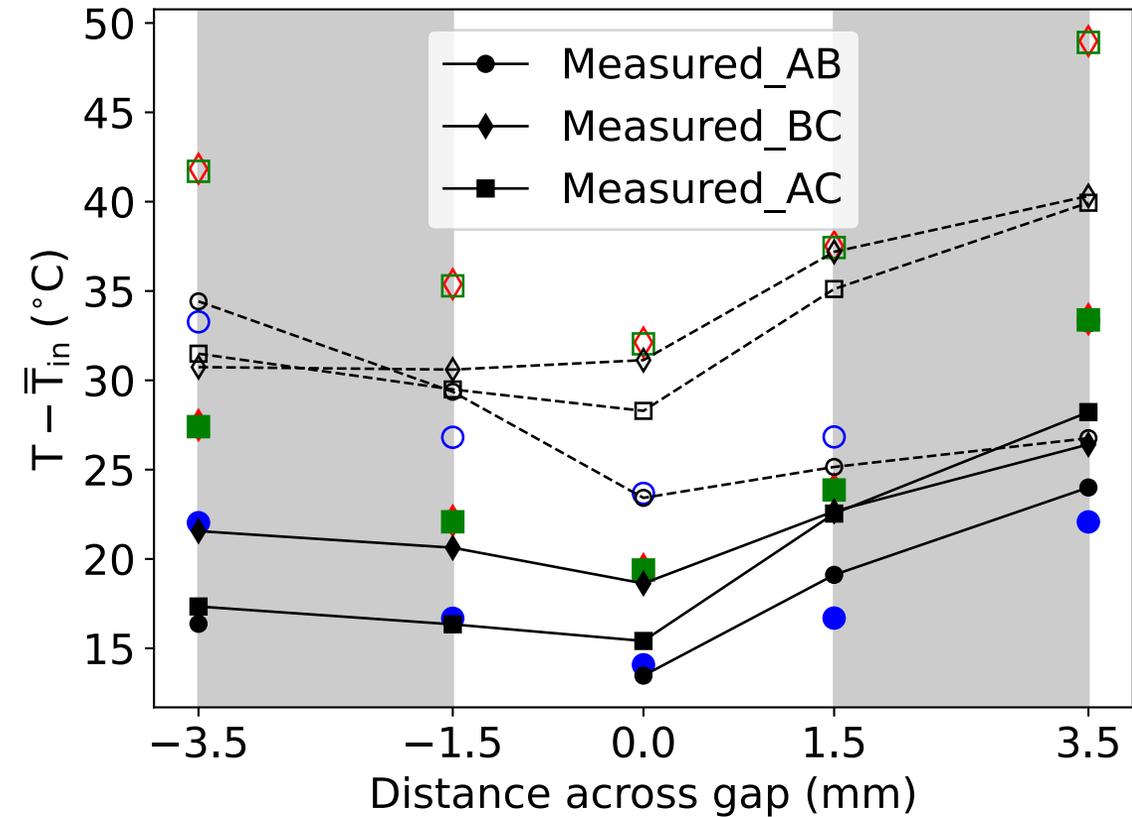
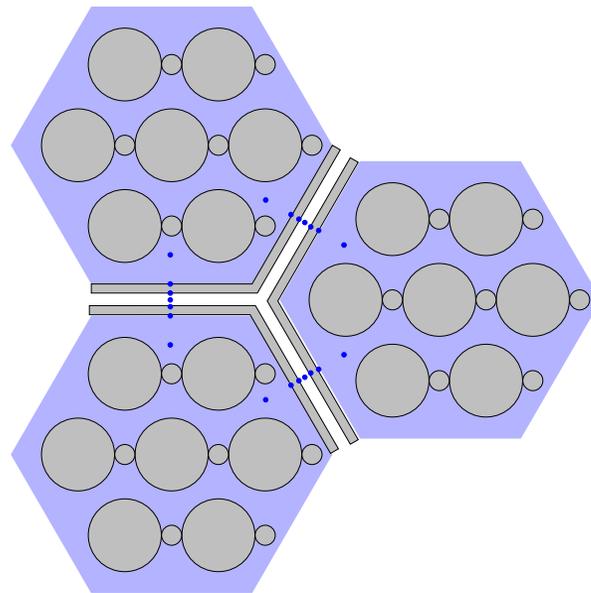


# Aymmetric case #55: radial temperature profiles

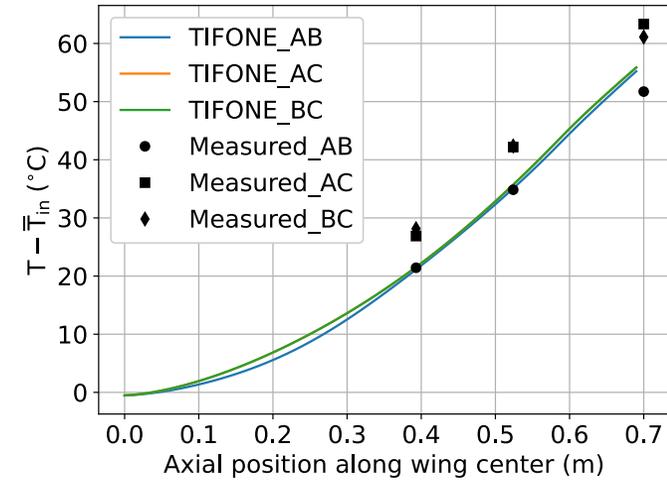
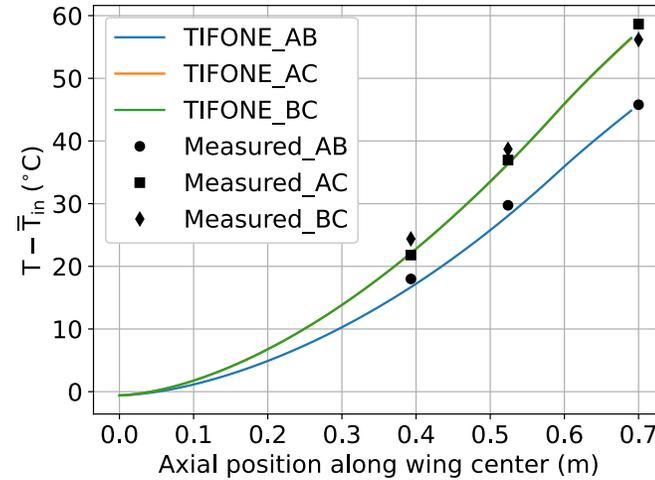
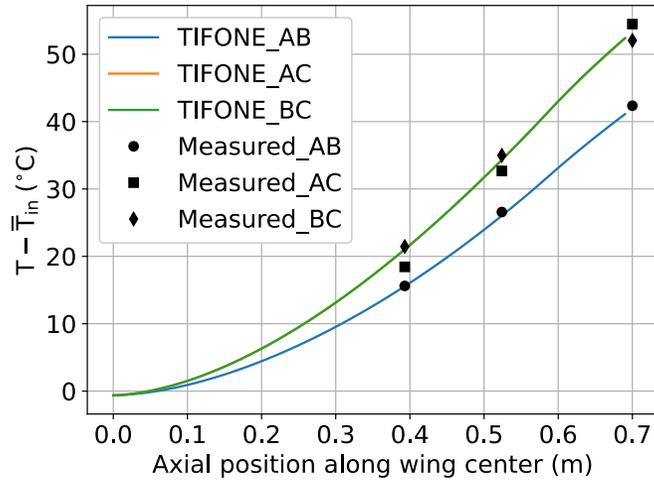
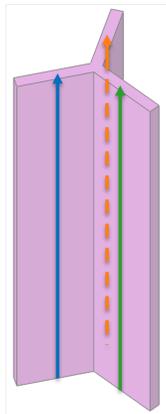
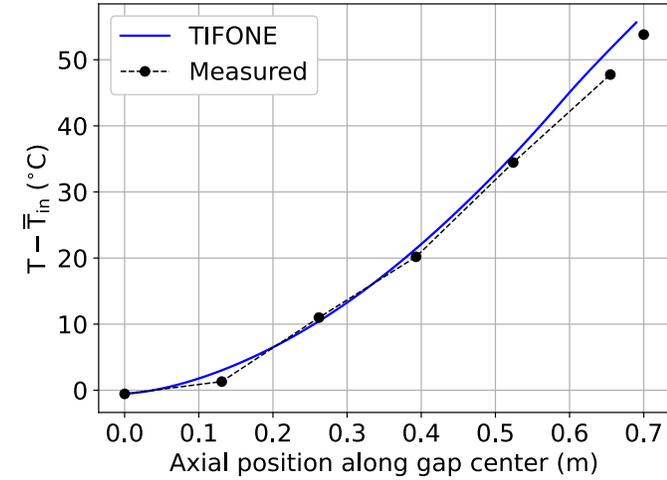
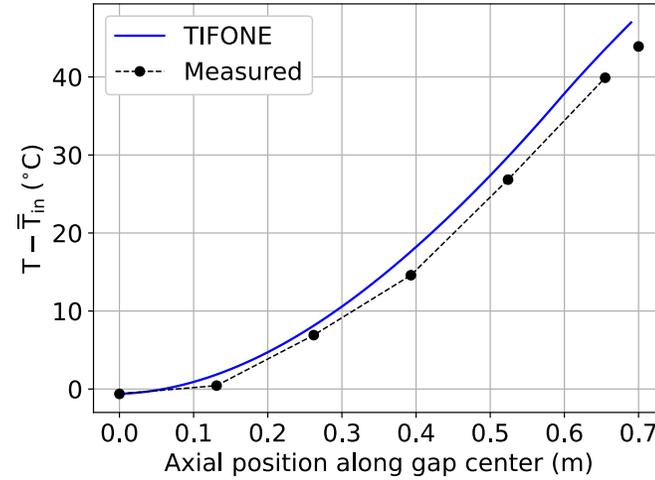
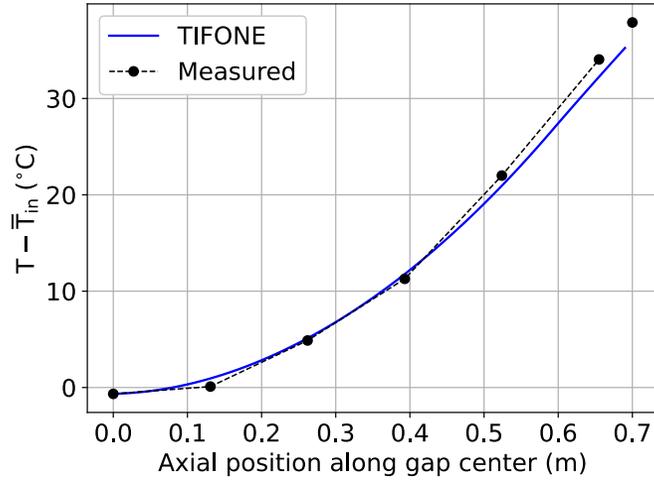
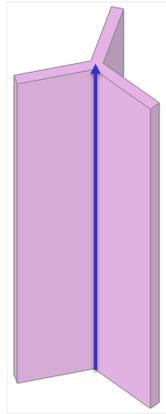




# Aymmetric case #55: radial temperature profiles



# Asymmetric cases # 57,59,61: axial temperature profiles



# Asymmetric cases # 57,59,61: radial temperature profiles

